

Hydrocarbon Behavior at Nanoscale Interfaces

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INTRODUCTION

Throughout Earth's crust and upper mantle, fluids play the dominant role in transporting and concentrating Earth's energy and mineral resources (Liebscher and Heinrich 2007). Furthermore, the flux of fluids, which act as both reaction media and reactants, strongly influences the genesis and evolution of many different kinds of rocks. Among many different types of fluids, those containing volatile carbon, hydrogen and oxygen (C-H-O) species tend to dominate in the lithosphere along with various electrolytes and silica. These fluids commonly contain methane as both a major constituent and an important energy source. Conventional natural gas deposits reside in sedimentary basins where fluid overpressure often results in brittle failure of the confining rocks. Industry exploration and exploitation of shale gas (e.g., the Marcellus, Utica, and Barnett formations) has refocused attention on understanding the fundamental behavior of volatile hydrocarbon—rock interactions. Recent observations of hydrocarbons emanating from non-sedimentary systems (abiogenic), such as mid-ocean ridge hydrothermal systems or occurring within some crystalline rock-dominated Precambrian shield environments have challenged the view that organic rich sediments provide the only significant source of crustal hydrocarbons (Potter and Konnerup-Madsen 2003; Sleep et al. 2004; Sherwood Lollar et al. 2006; McColom 2013; Sephton and Hazen 2013). Geopressured-geothermal regimes contain C-H-O fluids with vast energy potential in the form of methane and hot water at high pressure. Even fluid inclusions from both metamorphic and igneous terrains record the presence of methane-bearing fluids reflecting reduced redox state conditions of formation.

The consequences of coupled reactive-transport processes common to most geological environments depend on the properties and reactivity of these crustal fluids over broad ranges of temperature, pressure and fluid composition. The relative strengths of complex molecular-scale interactions in geologic fluids, and the changes in those interactions with temperature, pressure, and fluid composition, are the fundamental basis for observed fluid properties. Complex intermolecular interactions of C-H-O-N-S fluids (H₂O, CO₂, CH₄, H₂, H₂S, N₂) result in their unique thermophysical properties, including large deviations in the volumetric properties from ideality, vapor-liquid equilibria, and critical phenomena. Indeed, a key goal in geochemistry is to develop a comprehensive understanding of the thermophysical properties, structures, dynamics, and reactivity of complex geologic fluids and molecules (water and other C-H-O-N-S fluids, electrolytes, and organic-biological molecules) at multiple length scales

(molecular to macroscopic) over wide ranges of temperature, pressure, and composition. This knowledge is foundational to advances in the understanding of other geochemical processes involving mineral-fluid interfaces and reactions. It is also becoming increasingly clear that organic molecules present as gas species, in aqueous and mixed-volatile fluids—ranging from simple hydrocarbons and carboxylic acids to branched and cyclic compounds, to proteins and humic substances—play major roles in controlling geochemical processes, not just at Earth's surface, but also deep within the crust. The origin of life may be partly attributable to the properties of such molecules in complex fluids under extreme conditions, as they appear to play an important role in mineral reactivity and templating of mineral precipitates.

Hydrocarbons (e.g., CH₄, C₂H₆, etc.), CO₂, and aqueous solutions can occupy the pores or fractures of numerous types of complex heterogeneous Earth materials present in the systems outlined above. This accessible porosity within the solids can span wide length scales (d as pore diameter or fracture aperture) including micro-, meso-, and macroporous regimes ($d < 2.0$ nm, $2.0 < d < 50$ nm, and $d > 50$ nm, respectively, as defined by IUPAC). Porous solid matrices include rock or soil systems that contain clays and other phyllosilicates, zeolites, coal, graphite, or other carbonaceous-rich units; and weathered or altered silicates (e.g., feldspar to clay; olivine to serpentine), oxides, and carbonates. Examples of micro- and mesoporous features in natural solids and synthetic engineered proxies for natural materials are given in Figure 1. A number of factors dictate how fluids, and with them reactants and products of intrapore transformations, migrate into and through these nano-environments, wet, and ultimately adsorb and react with the solid surfaces. Factors include the size, shape, distribution, and interconnectedness of confined geometries, the chemistry of the solid and the fluids, and their physical properties (Cole et al. 2004). The dynamic behavior of fluids and gases contained within solids is controlled by processes occurring at the interface between the various phases (e.g., water-water, water-solute, water-volatile, water-solid, solute-solid, volatile-solid, etc.), as well as the rates of supply and removal of mobile constituents.

There is general agreement that the collective structure and properties of bulk fluids are altered by solid substrates, confinement between two mineral surfaces, or in narrow pores due to the interplay of the intrinsic length scales of the fluid and the length scale due to confinement (Gelb et al. 1999). However, compared with the effort expended to study bulk fluids, a fundamental understanding of the thermodynamic, structural and dynamic properties of volatile C-H-O fluids in nano-confined geometries, and their influence on the properties of the porous solid, is much less evolved, particularly for natural mineral substrates. Examples

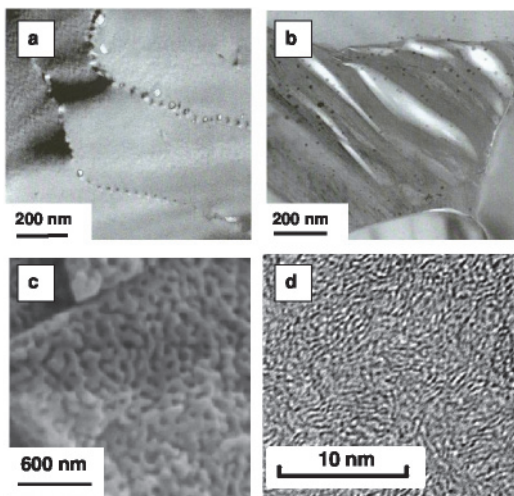


Figure 1. Electron microscopy images of micro- and mesoporous Earth and engineered materials: (a) pores along grain boundaries in weakly weathered basalt, (b) clay formation with large pores (white areas) at a grain boundary intersection in altered basalt, (c) controlled-pore glass, and (d) slit-like pores in carbon fiber monolith. [Used with kind permission of Springer Science+Business Media from Cole et al. (2009) *Neutron Applications in Earth, Energy and Environmental Sciences*, Fig. 1, p. 544.]

of experimental and computational efforts relevant to the behavior of Earth materials (defined as gases, solutions, and solids) include the study of CO₂ in thin pores (Belonoshko 1989), water structure and dynamics in clays (Skipper et al. 1995; Pitteloud et al. 2003; Wang et al. 2003; Skipper et al. 2006), ion adsorption into alumina mesoporous materials (Wang et al. 2002), and water within layered silicates at elevated pressure and temperature (Wang et al. 2004, 2005, 2006). These studies (and numerous others cited in Cole et al. 2006, 2009, 2010) demonstrate that a fluid can exhibit nano-confinement promoted phase transitions, including freezing, boiling, condensation, and immiscibility, which are intrinsic to the fluid-confining surface interactions (such as wetting and layering). Also crucial to the molecular behavior of fluids is the geometry of the pore, which can include simple planar walls (slits) such as encountered in clays and micas; cylinders, and spheres; and spheres linked with cylinders as observed in zeolites. Other factors that contribute to the modification of fluid properties include the randomness of the matrix and the connectivity of the pore network.

Given the complexity of natural C-O-H fluids and their roles in mediating surface interactions and reactivity with mineral phases, there can be no doubt that a quantitative understanding is needed of molecular-level fluid properties and fluid interactions with solids. A wide spectrum of analytical approaches can be brought to bear on Earth materials and engineered proxies, including, but certainly not limited to dynamic light scattering, IR, microscopy (e.g., electron; force), NMR, synchrotron-based X-rays, and neutron scattering and diffraction. When coupled with molecular simulation, this wide array of methods provides the means to which we can interrogate the structure and dynamics of fluids and their interactions with solids. Each of these methods provides a unique window into the properties and behavior of fluids and their reactivity. The inherent advantage of using engineered proxies for Earth materials is two-fold: (a) the mathematical rendering of details of the solid structure for simulation purposes is more straightforward when using synthetic materials and (b) interpretation of experimental results is less cumbersome.

The objective of this chapter is to provide fundamental, molecular- to microscopic-level descriptions of the sorptivity, structure, and dynamics of hydrocarbon (HC)-bearing fluids at mineral surfaces or within nanoporous matrices. The emphasis is on non-aqueous systems. Wherever possible we highlight results obtained from higher temperature-pressure sorption experiments, neutron scattering, NMR, and molecular-level modeling that have relevance to the deeper carbon cycle, although such studies are not common. We will not focus on the voluminous literature describing the behavior of hydrocarbons on activated carbon, carbon nanotubes, coal, synthetic gas storage materials such as metal-organic frameworks, and polymers. Rather we will emphasize key experimental and modeling results obtained on oxides and silicates, and synthetic engineered equivalents such as meso- and microporous silica and certain zeolites [the reader is referred to the book by Kärger et al. (2012) for more in-depth coverage of fluid behavior in zeolites]. We will assume as a first approximation that these engineered substrates act as reasonable proxies for the Earth materials. To best capture the behavior of hydrocarbons on mineral substrates or within nanoconfined volumes, we will address three key subtopics:

1. Adsorption-desorption behavior of methane and related HC fluids (and their mixtures) on a variety of substrates and in nanoporous matrices that yield microstructural insights,
2. Dynamical behavior of methane and related HC volatiles at mineral surfaces and within nanopores with and without surface H₂O present,
3. Molecular-level modeling results that provide important insights into the interfacial properties of these mineral-volatile systems, assist in the interpretation of experimental data and predict fluid behavior beyond the limits of current experimental capability.

Probing C-O-H behavior with neutron scattering and NMR

The properties of neutrons make them an ideal probe for comparing the properties of bulk hydrocarbons with those filling confined geometries (Pynn 2009). Neutrons can be scattered either coherently or incoherently, thus providing opportunity for various kinds of analysis of both structural and dynamic properties of confined liquids. Such analysis is possible due to the fact that the wavelengths of thermal and cold neutrons are comparable with intermolecular distances in condensed phases, while the neutron energy can be tailored to probe both high-(collective and single-particle vibrational) and low-frequency (single-particle diffusive) motions in the system. Importantly, the large incoherent scattering cross section of hydrogen compared to other elements allows obtaining scattering spectra dominated by the scattering from hydrogen-containing species (see recent review article by Neumann (2006)), whereas the X-ray scattering from such systems, which is virtually insensitive to hydrogen, would be dominated by the signal from the confining matrix. Last but not least, the large difference in the coherent and incoherent neutron scattering cross sections of hydrogen and deuterium allows selection of atoms to dominate the scattering signal by means of deuteration of the fragments of liquid molecules or the confining matrix.

Nuclear magnetic resonance (NMR) is a resonance concept between magnetization of nuclear spins and magnetic radio-frequency waves (Abragam 1961; Ernst 1987). NMR is employed in order to study local molecular properties of matter in detail regardless of the state of the system. One of the primary “fingerprints” of local structure probed by solid-state NMR is the chemical shielding, usually measured as the “chemical shift,” which is the difference in NMR resonance frequency of the species of interest from that of a known reference compound. Isotropic chemical shifts are indicative of local environment, and are often tabulated with typical ranges given for specific types of local bonding environments. For example, ^{29}Si nuclei in silicon atoms bound through three bridging oxygen atoms to other silicon atoms and one oxygen that is part of a hydroxyl group are typically found in the range of -110 to -120 ppm of shift from the reference of a tetramethylsilane molecule in neat solution. However, when proposed chemical species are difficult to identify by shift alone, multiple-resonance NMR methods (Pantano et al. 2003) are used to probe and compare to quantum chemical calculations (Fry et al. 2006; Johnston et al. 2009) for determination of local ordering.

Many of the chemistries of interest in hydrocarbon systems will occur at surfaces of materials and “surface selective” NMR will aid in the understanding of adsorption and reactivity. Hydrocarbons whose under-confinement behaviors have been investigated by NMR include benzene, derivatives of benzene, diethyl ether, methane, and acetone (Stallmach et al. 2001; Krutyeva et al. 2007; Xu et al. 2007). These hydrocarbons and their derivatives were confined into various porous systems such as mesoporous and nanoporous MCM-41 (Stallmach et al. 2001; Xu et al. 2007), mesoporous Vycor glass (Dvoyaskin et al. 2007), trimethyl-silylized nanoporous silica gel (Fernandez et al. 2008), and silicate zeolite (Pampel et al. 2005). The first important issue regarding porous system surface characterization is the utilization of solid-state magic angle spinning (MAS) NMR. In MAS NMR, the effect of molecular dynamics on the NMR interactions is mimicked by fast sample spinning around an axis, including the “magic angle” of 54.7° with the external applied magnetic (B_0) field. Fast sample spinning such as MAS NMR experiments removes most anisotropic nuclear interactions leading to line broadening in NMR spectra of solids. Nowadays, typical rotation speeds are in the range of 10-70 kHz with various outer diameter rotors of 7 mm to 1.5 mm (Xu et al. 2007; Vogel 2010). Solid-state MAS NMR on porous systems include, for instance, quantifying accessible hydroxyl sites of porous surfaces (Fry et al. 2003; Pantano et al. 2003). The detection of specific species on the surfaces of materials is often accomplished with heteronuclear correlation methods such as cross-polarization (Fry et al. 2003, 2006; Tsomaia et al. 2003) or J-coupled NMR spectroscopy. Surface selective spin correlation methods can be used on both raw samples and these same

samples during and after contact with fluids of interest to map out possible reactive structures as well as reaction products or sites depleted by interactions with the alkane species. NMR studies of the alkanes themselves, as well as any water or CO₂ incorporated with the alkanes, will focus on studies of chemical shift—primarily ¹³C and ¹H—as well as spin relaxation and diffusion experiments using these same nuclides. Demonstrated efforts (Riehl and Koch 1972) have revealed the depth of information available from systematic measurements of longitudinal and transverse spin relaxation rates ($1/T_1$ and $1/T_2$, respectively) as well as diffusion coefficients (Dawson et al. 1970; Helbaek et al. 1996). In NMR experiments, upon the application of radio-frequency pulses to disturb the magnetization of nuclear spins, the equilibrium distribution state is reestablished by relaxation processes. The longitudinal relaxation time T_1 and transversal magnetization time T_2 are the magnetization components parallel and perpendicular to external magnetic field B_0 , respectively. T_1 is an energy driven process, while T_2 is governed by entropy. Both T_1 and T_2 are important parameters to be measured since they are traditional ways to study molecular reorientations (Abragam 1961; Vogel 2010).

NON-AQUEOUS FLUID ADSORPTION BEHAVIOR: EXPERIMENTAL

Background on adsorption concepts and approaches

The interaction of short-length linear alkanes including methane, ethane, propane, and *n*-butane and their mixtures with high surface area solids has received considerable attention over many decades, driven largely by the separations and catalysis communities. Substrates that have received the most attention include various types of carbon (e.g., activated carbon, carbon black, carbon fibers, and coal; Jiang et al. 2005), pillared clays (Li et al. 2007), clathrates (Roman-Perez et al. 2010), and zeolites, both natural and synthetic (Denayer et al. 2008). More recently synthetic materials such as micro- and mesoporous silica and metal-organic frameworks have been used to adsorb selectively light hydrocarbons from various gas mixtures.

Precise determination of adsorption/desorption isotherms at geological conditions is key to identifying surface-fluid interactions. Sorption measurements (volumetric, gravimetric, and calorimetric) are important because they provide valuable insights into the interfacial interactions between the solid substrate and the fluid phase. The magnitude of adsorption, the shape of the adsorption isotherm, and the presence or absence of hysteresis and its magnitude reveal a great deal about the properties of the surface, adsorbate molecule configurations, and the interactions between both adsorbate molecules themselves and with the substrate (Rouquerol et al. 1999; Myers and Monson 2002). Volumetric or gravimetric-based isotherms provide the most direct measure of such interactions to which other structural data, such as small angle neutron scattering (SANS) and neutron reflectivity (NR), can be compared. In most cases, however, these types of measurements are conducted at low temperature and modest pressures. Various kinds of carbon-based porous materials, zeolites, and modified organic frameworks are widely studied for methane adsorption (Zhang et al. 1991; Menon and Komarneni 1998; Cavenati et al. 2004; Wu et al. 2009). Carbon-based materials are more efficient adsorbents compared to zeolite on a weight basis. The reverse trend is observed on a volume basis because of the high solid density of zeolites (Zhang et al. 1991). Few studies explored the effect of moisture on adsorption capacity relative to methane (Clarkson and Bustin 1996; Rodriguez et al. 1997). Adsorption of methane and wet hydrocarbon gases on natural clays is rarely studied due to lower adsorption capacity of natural minerals (Stoessel and Byrne 1982). Pires et al. (2008) studied the selective adsorption of CO₂, methane, and ethane on porous clay heterostructures at ambient temperature and demonstrated that alkanes adsorb proportionally to free volume of adsorbent but CO₂ shows an inverse trend. This anomalous behavior is attributed to clay composition as well as specific interactions of CO₂ with the surface. Cheng and Huang (2004) have reported a comparative study of adsorption of C₁-C₆ hydrocarbons in gas mixtures on a variety of clays

and organic matter at lower pressures and temperatures up to 80 °C. This study confirms that despite the lower adsorption capacity for clay surfaces compared to coal substrates, the amounts adsorbed are significant (50–75% of the amount sorbed on coal). Similarly, few studies have been published on adsorption of methane and other hydrocarbon gases on natural silica (Wu et al. 1994). Although various studies discuss adsorption of CO₂ on coal substrates, zeolites, assorted metal oxides, and modified silica/clays, a limited number have tried to study CO₂ adsorption on natural minerals (e.g., Yong et al. 2002) particularly in the presence of water and aqueous carbonate species (e.g., Villalobos and Leckie 2000).

While adsorption-desorption phenomena have been the focus of many of these studies issues such as rates of sorption and transport behavior (diffusivity) have also been addressed (Schloemer and Krooss 2004; Kim and Dauskardt 2010). Techniques that have been used in these kinds of studies include but are not limited to volumetric and gravimetric sorption isotherm measurements, differential scanning and micro-calorimetry (DSC), NMR, FTIR, scattering (light, X-ray, and neutrons) and diffraction (X-ray, neutrons). For the most part these studies involve either high pressure at cryogenic to near-ambient temperature conditions or the converse, high temperature, but low pressures (few MPa). The use of extreme conditions of temperature and pressure is limited by the availability of novel high temperature-pressure sorption apparatus such as Rubotherm's magnetic suspension balance and appropriate high pressure-temperature scattering sample cells for *in situ* interrogation. Molecular dynamics, Monte Carlo, and *ab initio* methods are widely used to predict sorption and transport behavior (Combariza et al. 2011; Krishna and van Baten 2011) and/or help interpret experimental data (Lithoxoos et al. 2010). Collectively, results from these studies (and many more not formally cited) provide an important framework for gaining a fundamental understanding of the interfacial behavior of the light hydrocarbons interacting with synthetic "Earth" proxies, as well as natural mineral and rock matrices at conditions relevant to shallow crustal settings; ~200 °C and 100 MPa. However, to our knowledge, with the possible exception of coal, there has not been a systematic study of the effects of temperature, pressure, variable pore size, shape, roughness, and connectivity, and degree of surface hydrophobicity on light hydrocarbon-mineral interaction relevant to subsurface fine-grained sedimentary lithologies. Further, fundamental understanding of interfacial behavior involving interactions between hydrocarbons and aqueous films on minerals is very poor compared to studies that have explored H₂O wetting phenomena (e.g., Fenter 2002), and the role of confinement, surface charge, and electrochemical reactions on surface forces at mineral surfaces (e.g., Alcantar et al. 2003; Anzalone et al. 2006; Greene et al. 2009).

Behavior of hydrocarbons and related C-O-H fluids in the presence of complex solution chemistry (e.g., elevated electrolyte concentrations; silica) at elevated temperatures and pressures is obviously of more relevance to our understanding of the deep carbon cycle. A number of sorption studies have been performed on supercritical and near-critical fluids, mainly using volumetric techniques. Experimental adsorption isotherms obtained over wider ranges of pressure extending to compressed liquid or dense supercritical fluid revealed effects that were not present or could be neglected in low-density gas adsorption. Pronounced high-pressure depletion effects over a large region of fluid densities have been reported for argon, neon, krypton, nitrogen, and methane physisorbed to activated carbon (Malbrunot et al. 1992). Thommes et al. (1995) studied the sorption of supercritical SF₆ to mesoporous CPG-10 silica and found adsorption at low fluid density, but a strong decrease of the adsorbed amount of fluid in the vicinity of the critical point, and named the effect *critical depletion*. Rayendran et al. (2002) report the occurrence of critical depletion for N₂O sorption to silica gel. Several theoretical and simulation studies have been published on critical/high-density depletion phenomena (Maciolek et al. 1999; Brovchenko et al. 2004, 2005; Oleinikova et al. 2006; Brovchenko and Oleinikova 2008), with partly conflicting results. Part of the problem is that the common quantity measured in sorption experiments, excess adsorption, gives only the net sorption effect, but cannot provide a microscopic picture of the fluid-substrate interactions.

Observationally as one traverses from low to high density, the experimental adsorption isotherms for C-O-H fluids can exhibit a maximum at the density of bulk fluid approaching its critical value (Parcher and Strubinger 1989; Strubinger and Parcher 1989; Aranovich and Donohue 1998; Donohue and Aranovich 1999). At still higher densities, experimental excess adsorption isotherms may reach zero or even negative values. This behavior is independent of any additional volumetric effects, such as adsorbent swelling or deformation at elevated pressure. The decrease of the amount adsorbed with pressure may appear counterintuitive by implying a mechanical instability of the system. However, the quantity measured by all conventional methods does not represent the total amount of fluid present in the vicinity of solid surface but instead the excess adsorption (Gibbs surface excess; Fig. 2)—the difference between the actual amount of fluid contained inside a pore system and the hypothetical amount of fluid at bulk density filling the pore spaces, i.e. in absence of fluid-solid interactions.

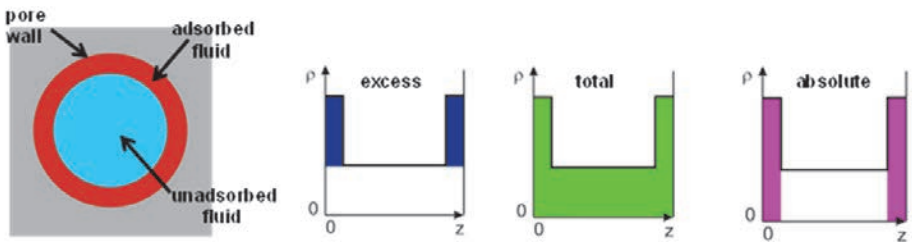


Figure 2. Schematic of a single pore (left panel) showing the adsorbed phase (red) and the unadsorbed fluid (blue). Also shown are the three types of sorption described in the text – excess, total and absolute. ρ refers to fluid density and z is the diameter of the pore. (G. Rother, pers. commun.)

C-O-H pore fluid densities

As noted above, excess adsorption, which can be measured without the knowledge of any microscopic properties of the adsorbed phase, is an important quantity used for thermodynamic analysis of many aspects of adsorption and is routinely used in modeling and control of technological processes (Sircar 1999). However, the properties of the adsorbed phase, including the average density of the pore-filling fluid, are essential in quantifying fluid-rock interactions in systems dominated by nano- to microscale pore features (Rother et al. 2007). Gruszkiewicz et al. (2012) reported results on propane (C_3H_8) and CO_2 obtained from a novel high temperature-high pressure vibrating tube densimeter (VTD) capable of measuring pore fluid density and total adsorption capacity in mesoporous solids. The densities were determined for propane at subcritical and supercritical temperatures (between 35 °C and 97 °C) and carbon dioxide at supercritical temperatures (between 32 °C and 50 °C) saturating hydrophobic mesoporous silica aerogel (0.2 g/cm³, 90% porosity) synthesized inside Hastelloy U-tubes (Fig. 3). In this method the porous solid completely fills the tube, so that virtually no bulk fluid outside of the pore system is present in the measurement zone; i.e., the contact with the bulk fluid reservoir occurs outside of the vibrating cantilever. The mass of the pore fluid, proportional to its average density, is measured directly as the inertia of the cantilever containing the solid sample imbedded with fluid. Additionally, supercritical isotherms of excess adsorption for CO_2 and the same porous material were measured gravimetrically using a precise Rubotherm magnetically-coupled microbalance.

The densities of pore-filling propane measured at four subcritical temperatures (35, 70, 92, and 95 °C) and at 97.0 °C, about 0.3 °C above the critical temperature ($T_c = 96.7$ °C) are given in Figure 4 plotted against pressure. Also shown are the densities of bulk fluid calculated from the equation of state (Span and Wagner 1996; Lemmon et al. 2010). Pore fluid densities and

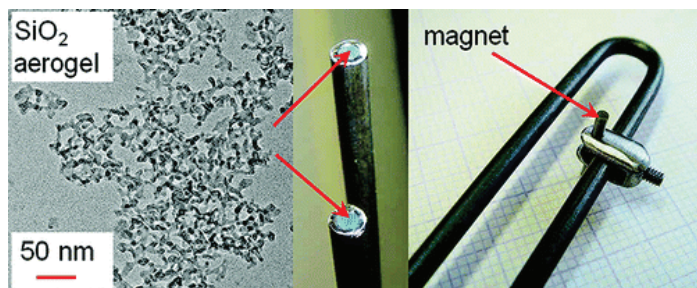


Figure 3. A transmission electron microscopy (TEM) image of the silica aerogel structure (silica strands are darker), the Hastelloy U-tube with the silica aerogel synthesized inside, and magnet clamp attached to the U-tube. [Used by permission of the American Chemical Society © 2012, from Gruskiewicz et al. (2012) *Langmuir*, Vol. 28, Fig. 1, p. 5073.]

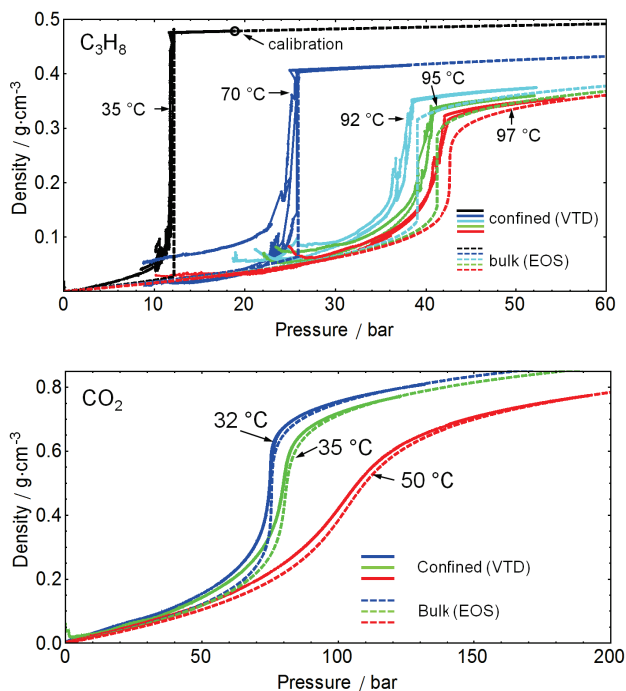


Figure 4. (top) Subcritical (35 °C, 70 °C, 92 °C, and 95 °C) and supercritical (97 °C) isotherms of confined fluid density for propane in silica aerogel. (bottom) Supercritical (32, 35 and 50 °C) isotherms of confined and bulk fluid density for carbon dioxide in silica aerogel. [Used by permission of the American Chemical Society © 2012, from Gruskiewicz et al. (2012) *Langmuir*, Vol. 28, Fig. 4, p. 505 (top panel), Fig. 6, p. 5076 (bottom panel).]

total adsorption isotherms increased monotonically with increasing density of the bulk fluid, in contrast to excess adsorption isotherms, which reached a maximum and then decreased towards zero or negative values above the critical density of the bulk fluid (Fig. 4). Compression of the confined fluid significantly beyond the density of the bulk fluid at the same temperature was observed even at subcritical temperatures. The isotherms of confined fluid density and excess adsorption (not shown) contain complementary information. For instance, the maxima

of excess adsorption occur below the critical density of the bulk fluid at the beginning of the plateau region in the total adsorption, marking the end of the transition of pore fluid to a denser, liquid-like pore phase. No measurable effect of pore confinement on the liquid-vapor critical point was found. The results for propane and carbon dioxide showed similarity in the sense of the principle of corresponding states. Good quantitative agreement was obtained between excess adsorption isotherms determined from VTD total adsorption results and those measured gravimetrically at the same temperature, confirming the validity of the vibrating tube measurements. The flatter initial slopes exhibited in the propane isotherms are indicative of relatively weak fluid-pore wall interactions. The step increase in density at higher pressures can be indicative of pore condensation and/or stronger fluid-fluid interactions. The somewhat steeper initial slopes associated with lower pressures observed for the CO_2 are typical for a fluid that experiences a somewhat stronger fluid-pore wall interaction compared to propane.

To better compare these results and to emphasize the corresponding states' similarity between the fluids, the results are also shown in Figure 5 in terms of reduced densities, $\rho_r = \rho/\rho_c$, where $\rho_c = 0.220 \text{ g/cm}^3$ for C_3H_8 and $\rho_c = 0.4676 \text{ g/cm}^3$ for CO_2 . The diagonal dashed straight line in Figure 5 represents the hypothetical condition where the confined fluid density is equal to the bulk fluid density; the deviations of the experimental isotherms from this line represent the excess density due to solid-fluid interactions. This figure demonstrates that the confined fluid densities, and consequently total adsorption isotherms, are non-decreasing functions of increasing bulk fluid density. Each of the subcritical isotherms features a plateau formed by a straight tie line extending between the densities of bulk vapor and liquid phases in equilibrium. The dotted curve in Figure 5 represents the vapor-liquid equilibrium envelope of bulk propane with the densities of the phases in equilibrium and the bulk fluid critical point marked with symbols.

Hydrocarbon-interfacial microstructure

As noted previously, the sorption of gaseous subcritical fluids on solid substrates has been studied extensively (Schreiber et al. 2002; Sel et al. 2007), while only a few studies exist on the nanoscale structure and dynamics of interfacial fluids, and almost nothing is known about the interfacial properties of near-critical and supercritical fluids. In the context of hydrocarbons, this is an important P - T regime because these fluids will be present at supercritical conditions. A poorly constrained yet fundamentally important fluid behavior has been identified wherein at P - T -density conditions below the critical point, fluid volume and density increase as the critical point is approached, while above the critical density fluid volume remains essentially constant but density decreases—the so-called fluid depletion effect where negative values of excess adsorption are estimated (Malbrunot et al. 1992; Thommes et al. 1995; Rajendran et al. 2002). However, theoretical and simulation efforts to model these data give conflicting results

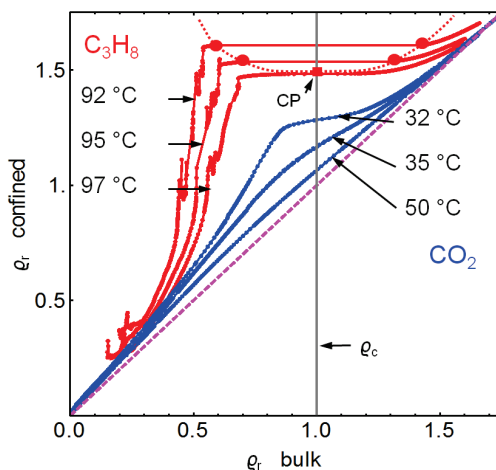


Figure 5. Total confined fluid reduced density (g/cm^3) isotherms for C_3H_8 and CO_2 plotted as a function of bulk fluid reduced density. [Used by permission of the American Chemical Society © 2012, from Gruszkiewicz et al. (2012) *Langmuir*, Vol. 28, Fig. 7, p. 5077.]

(Maciolek et al. 1998, 1999; Brovchenko et al. 2004, 2005; Oleinikova et al. 2006), which is due to the lack of experimental micro-structural characterization.

Many studies deal with the properties of fluids and fluid mixtures imbibed in the pores of engineered nanoporous materials. Porous silica (SiO_2) is frequently chosen because it can be synthesized with well-defined pore sizes in the range of less than 1 nm up to several tens of nm. The structural properties of confined liquids can be assessed using coherent scattering techniques, neutron diffraction (ND), and small-angle neutron scattering (SANS). The former allows one to measure the static structure factor, $S(Q)$, which can be then Fourier transformed to obtain the radial pair-distribution function, $g(r)$, that describes the distribution of the distances between the coherently scattering nuclei in the liquid. While ND measurements of liquids in confinement probe structural correlations not exceeding a few molecular diameters, SANS measurements provide coverage over much broader range in the real space (Radlinski 2006; Triolo and Agamalian 2009). This is because SANS involves measuring neutron intensities at very low values of the scattering vector, Q (i.e., at small angles).

SANS has been widely used in the study of fluid behavior in porous media and recently became the first technique capable to quantify the sorption properties of C-O-H fluids in porous media in terms of the mean density and volume of the adsorbed phase (Rother et al. 2007). In this study, the sorption properties of supercritical deuterated propane and CO_2 in silica aerogel with 96% porosity and pores ranging from 20-50 nm were investigated. SANS and neutron transmission data have been measured for fluid-saturated silica at different fluid densities and temperatures. The mean density ρ_3 and volume fraction ϕ_3 of the sorption phase were calculated from the SANS and neutron transmission data by application of a new model, which makes use of the three-phase model by Wu (1982) and a mass balance consideration of the pore fluid, which can be obtained from neutron transmission measurements or gravimetric sorption measurements. It was found that the fluid is adsorbed to the porous matrix at low fluid densities but depleted from the pore spaces at higher fluid densities (i.e., in the vicinity of the critical density and above). Figure 6 shows the evolution of the physical properties of the sorption phase, expressed in terms of ρ_3 as a function of temperature and (bulk) fluid density ρ_2 . The bulk critical density of deuterated propane is $\rho_c \approx 0.27 \text{ g/cm}^3$, and the critical temperature is $T_c \approx 91.0 \text{ }^\circ\text{C}$. The fluid density in the adsorbed phase is up to about three times higher than ρ_2 in the low-pressure region, while it remains constant and below ρ_2 at and above the critical pressure.

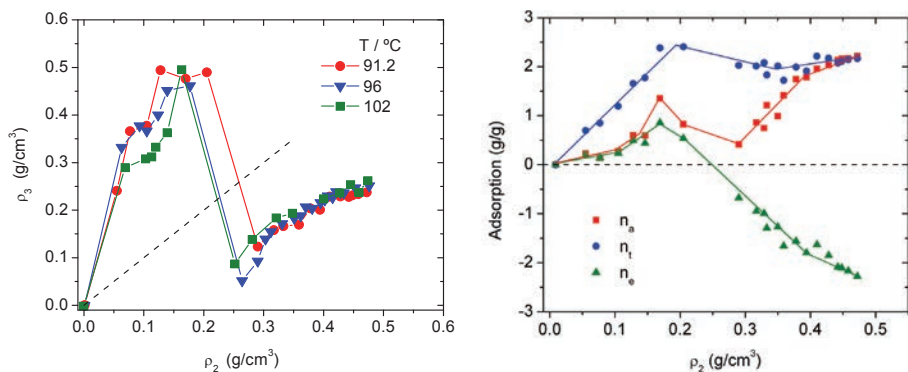


Figure 6. Results of SANS on deuterated propane inside silica mesoporous aerogel (0.1 g/cc) at three supercritical temperature from; (left) mean density ρ_3 of the sorption phase as a function of the density of the unadsorbed fluid; dashed line represents behavior for a fluid-porous solid system with no adsorption; (right) adsorption quantities calculated from the density and volume of the sorption phase. n_a = absolute adsorption; n_t = total adsorption; n_e = excess adsorption. [Used by permission of the American Chemical Society © 2007, from Rother et al. (2007) *J Phys Chem-C*, Vol. 111, Fig. 6, p. 15740 and Fig. 8, p. 15740.]

With the information on ρ_3 and ϕ_3 (not shown), calculation of the absolute adsorption, which is the relevant quantity for the application of the equation of adsorption and molecular modeling work, is possible without the introduction of further assumptions. The calculated values for the absolute adsorption (n_a), total adsorption (n_t) and excess adsorption (n_e) are given in Figure 6. The absolute adsorption is similar to the commonly measured excess adsorption only at low fluid densities but differ significantly at higher fluid densities. Cole et al. (2010) has been able to theoretically emulate the shape of this trend by using an integral equation approximation. From the sorption phase density and volume the excess sorption, total sorption and absolute sorption can be calculated. These neutron results have been compared to excess sorption data measured with gravimetric techniques and total sorption data measured with the vibrating tube densimeter (Rother et al 2012; Gruszkiewicz et al 2012). General agreement of the data has been found, verifying the validity of the neutron method.

In a related study, Kainourgiakis et al. (2010) studied the behavior of water, hexane, and hexane-water mixtures at ambient temperature imbibed in macroporous α - Al_2O_3 (34% porosity; ~ 180 nm pores; total pore volume of ~ 0.14 cm^3/g), using ultra-small angle neutron scattering (USANS). The intent was to quantify the multiphase pore-filling behavior of a wetting (water) and non-wetting fluid (hexane). They used a 7.3% $\text{H}_2\text{O}/\text{D}_2\text{O}$ mixture that matched the scattering length of the alumina matrix, which allowed the study of the contributions to the scattering signal of the individual phases in water-water and water-hexane systems, and the hydrocarbon in hexane-air systems. In the case of the water-loaded samples (and to a certain extent also when water-hexane mixtures are used) the progressive hydration leads towards the formation of larger water-hydrocarbon clusters. These clusters can be considered as biphasic "aggregates," comprising continuous solid- and water-rich regions, which nevertheless can be characterized as homogeneous in terms of scattering behavior since the 7.3% $\text{H}_2\text{O}/\text{D}_2\text{O}$ mixture used has the same scattering length density as alumina. This characterization is indeed confirmed by the practically zero intensity recorded when the pore space is fully occupied ($V_{\text{water}} = 1$) by the aqueous phase. On the other hand, the spectra of the samples impregnated with hexane exhibit, in practice, the same trend, while the slight variation of intensity is attributed to the reduced contrast achieved as increased quantities of the hydrocarbon are introduced in the pore network. Most interestingly, the autocorrelation function curves obtained from scattering for the cases of the partial filling (e.g., $V_{\text{water}} = 1/3$ or $2/3$ where V_s is defined as the fraction of total pore volume occupied by a certain fluid component) of the pore volume with only the aqueous phase and the complete saturation with an equivalent water-hexane mixture (i.e., $V_{\text{water}} = 1/3$ or $2/3$ and $V_{\text{hexane}} = 2/3$ or $1/3$) practically coincide despite the differentiation of the fluids occupying the pore volume and the significant variation therefore of the interfacial energies coupled in the respective systems. In practical terms this important observation provides direct experimental evidence that the spatial distribution of the fluid phases is related to their wetting/non-wetting relative behavior and is not affected significantly by the actual values of their particular interfacial properties. Simulations of this wetting process for different loadings are shown in Figure 7.

Zeolites are microporous aluminosilicate minerals that play an important role in many natural and industrial processes, including water purification through ion exchange, catalytic hydrocarbon cracking, and separation of pollutants from natural gas. They possess pore widths of typically a few tenths of a nanometer, making X-ray and neutron diffraction suitable tools for the study of these materials and guest molecules inside their pore systems. Neutron diffractometers exist in a variety of configurations for thermal and cold neutrons optimized for resolution or flux and interrogate length scales of up to 2 nm. The ND technique has been recently used by Mentzen to study the adsorption of hydrogen and benzene in MFI-type zeolites (Mentzen 2007). The positions of the guest molecules in the microporous host structure were determined through Rietveld analysis to define the binding sites. The sorption of several hydrocarbons, including heptane, in silicalite-1 zeolite was studied by Floquet et al. (2003,

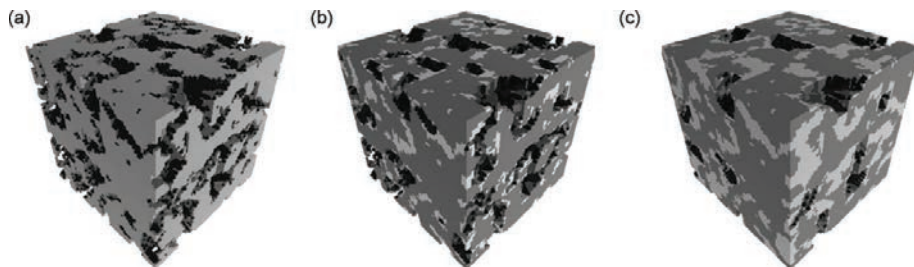


Figure 7. 3D simulation images of (a) dry alumina structure; (b) spatial distribution of a wetting fluid for $V_s = 1/3$ and (c) $V_s = 2/3$. Each block is approximately 500 nm on a side. [Used by permission of Elsevier © 2010, from Kainourgiakis et al. (2010) *Appl Surf Phys*, Vol. 256, Fig. 3, p. 5332.]

2007), who used ND. Their results indicate that heptane populates the straight channels of the silicalite pore network first, while the sinusoidal channels and intersections fill with heptane only above a heptane concentration of about 3.9 molecules per unit cell.

NON-AQUEOUS FLUID DYNAMICS AT INTERFACES: EXPERIMENTAL

Dynamical fluid behavior is controlled by processes occurring at the fluid-pore wall or fluid-fluid interface, as well as by the rates of supply and removal of mobile constituents. Key issues pertaining to these types of interactions that remain largely unresolved, particularly for conditions of elevated temperature and pressure, include the extent of possible hydrogen bonding, molecular translation and rotation, average times between molecular jumps, and self-diffusion, which involve specific interactions between neighboring molecules leading to preferred molecular orientation that are affected by reduced dimensionality and fluid-pore wall interactions (Cole et al. 2006, 2009). Of the techniques that are available, neutron scattering and nuclear magnetic resonance are probably the most heavily used to obtain dynamical information on hydrogen-bearing fluids, such as self-diffusion, translational, and rotational motion from hydrocarbon-matrix interactions. More specifically, Pulsed Field Gradient NMR (PFG-NMR) was the first “microscopic” method advanced for the measurement of diffusion in zeolites in the late 1970s. It allowed accessing molecular displacements down to 0.1–1 μm for times on the order of 1 ms and was thus instrumental in elucidating intracrystalline and intercrystalline transport phenomena for a wide variety of systems (Jobic and Theodorou 2007). Quasielastic neutron scattering (QENS) is a complementary method to NMR that tracks the diffusive motions that take place on the timescale of a pico- to nano-second, which corresponds to the energy scale from a fraction of μeV to several hundred μeV (Bee 2003). The more energetic (on the energy scale from several to several hundreds of meV) vibrational and librational modes are typically probed using dedicated neutron spectrometers with moderate energy resolution and reasonably high incident neutron energies. On the timescale of such spectrometers, rotational and translational motions are very slow and can be neglected. This type of measurement is known as inelastic neutron spectroscopy (INS). Compared to infrared spectroscopy, INS benefits from the absence of optical selection rules and the large incoherent scattering cross section of hydrogen.

QENS probe of hydrocarbons in nanopores

As noted above QENS is an excellent tool to probe the mobility of confined hydrogen-bearing fluids, the property affected the most by a confinement; a change by one to two orders of magnitude in the mobility of a confined liquid is common. QENS targets the signal from incoherently scattering nuclei such as H, leading to a description of self-diffusion. The signal

measured by a spectrometer as a function on neutron energy transfer, E , is a Lorentzian with a half-width at half maximum (HWHM) $\Gamma = \hbar D Q^2$, where Q is the momentum transfer to the particle in the scattering process and D is the diffusion coefficient (Cole et al. 2006). In general, QENS probes rotational and translational diffusive motions of molecules that result in the broadening of the elastic peak. In QENS measurements, the effects of faster vibrational and librational motions manifest themselves in the overall reduction of scattering intensities (Debye-Waller factor). It should be noted that knowledge of the resolution function and an extremely good energy resolution are of paramount importance in QENS. For this reason, time-of-flight and backscattering spectrometers built at cold neutron sources are frequently employed in this type of experiment.

Even though water has been by far the most extensively investigated medium in nanoconfinement, other fluids in confined environments such as methane and other alkanes have attracted some attention. The majority of studies using QENS to interrogate hydrocarbon dynamics have focused on behavior in a variety of synthetic silicas and zeolites. For example, Benes et al. (2001) presented QENS results on the temperature dependence (200 to 250 K) of methane self-diffusion and molecular rotation in microporous silica with pores smaller than 1 nm. The self-diffusion coefficients of translational motion range from $1.1 \times 10^{-8} \text{ m}^2 \text{ s}^{-1}$ at 200 K to $1.9 \times 10^{-8} \text{ m}^2 \text{ s}^{-1}$ at 250 K with an estimated activation energy of 4 kJ mol^{-1} . The isotropic rotation diffusion constant is on the order of 10^{11} s^{-1} . Jobic (2000a, b) described the dynamics of complex hydrocarbon molecules in confinement (linear and branched alkanes, for hydrocarbon chains up to C-14, confined in ZSM-5 zeolite, Fig. 8a). In ZSM-5 zeolite there are two types of channels consisting of ten-membered oxygen rings. The straight elliptical channels (0.57-0.52 nm) are interconnected by near-circular channels (0.54 nm) in a zig-zag fashion, and there are four channel intersections per unit cell. Because of the relatively large size of the confined molecules, the diffusion could be observed within the time window of a backscattering spectrometer only at high temperatures. Branched alkanes were found to diffuse much more slowly than linear alkanes. Mitra and Mukhopadhyay (2004) reported on the residence times (τ), mean jump length (l), and translational motion (D) of propane in Na-Y zeolite (Na:Al = 1.7). The Na-Y zeolite structure is made up of a network of tetrahedrally connected pores (a -cages) of diameter $\sim 1.18 \text{ nm}$. The pores are interconnected through windows of diameter $\sim 0.8 \text{ nm}$. A schematic of Na-Y zeolite structure is shown in Figure 8b. They compared the experimental results with MD as shown in Table 1. Mamontov et al. (2005) explored the diffusion and relaxation dynamics of benzene (C_6H_6) in oriented 5-nm nanochannels of chrysotile [$\text{Mg}_3\text{Si}_2\text{O}_5(\text{OH})_4$] asbestos fibers from 260 to 320 K (Fig. 9). The

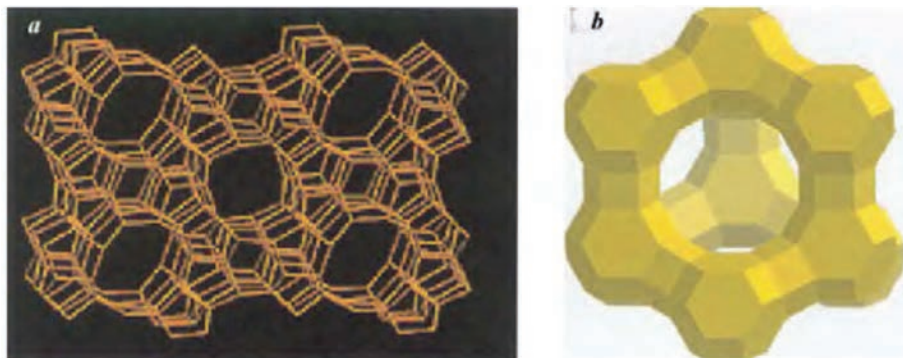
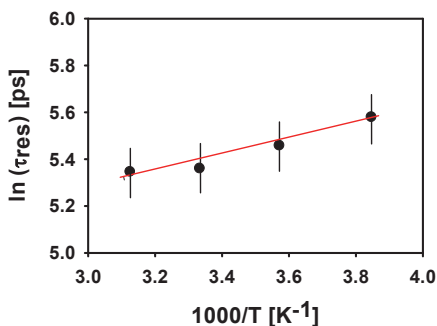
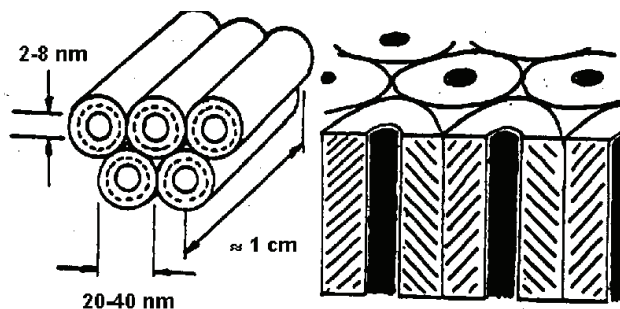


Figure 8. Schematic of cage pore structure in two commonly used zeolites (a) ZSM-5; channel diameter 0.52-0.57 nm and (b) Na-Y; channel diameter 0.8 nm. [Used by permission of Indian Academy of Sciences © 2003, from Mitra and Mukhopadhyay (2003) *Curr Sci*, Vol. 84, Fig. 3, p. 657.]

Table 1. Dynamical parameters for residence times (τ), jump length (l) and translational motion of propane adsorbed in Na-Y zeolite (Mitra and Mukhopadhyay 2004).

T (K)	τ (ps)	$(l^2)^{0.5}$ (nm)	D ($\times 10^{-5}$ cm ² s ⁻¹) QENS	D ($\times 10^{-5}$ cm ² s ⁻¹) MD
300	4.6 ± 0.5	0.25 ± 0.02	2.3 ± 0.3	3.6
324	4.3 ± 0.4	0.29 ± 0.02	3.2 ± 0.3	3.2
350	3.8 ± 0.3	0.30 ± 0.03	4.0 ± 0.4	3.0

**Figure 9.** (top) Schematic picture of a bundle of chrysotile asbestos fibers. (left) temperature dependence of the average residence time (τ) between translational diffusion jumps of benzene and its fit with Arrhenius law. [Used by permission of American Physical Society © 2005, from Mamontov et al. (2005) *Phys Rev E*, Vol. 72, Fig. 1, p. 051502-1, and Fig. 6, p. 051502-5. <http://link.aps.org/doi/10.1103/PhysRevE.72.051502>]

macroscopic alignment of the nanochannels provided an opportunity to study the anisotropy of the dynamics of a confined fluid by means of collecting the data with the scattering vector either parallel or perpendicular to the fibers axes. The translational diffusive motion of benzene molecules was observed to be isotropic. Diffusivities were not strongly temperature dependent and ranged from 0.88×10^{-10} m² s⁻¹ to 1.31×10^{-10} m² s⁻¹. Conversely, the residence times between translational jumps exhibited a weak temperature dependence (Fig. 9) and yielded a low activation energy of 2.8 kJ mol⁻¹.

A recent survey by Jovic and Theodorou (2007) provides an excellent overview of QENS studies of confined media in a number of zeolites and their synergy with molecular dynamic simulations. They compared the behavior of various alkanes in Al-Si-O-based zeolites with or without counterions such as Na (e.g., Si-only silicalite-1; Na-ZSM-5 [$Na_nAl_nSi_{96-n}O_{192} \cdot 16H_2O$ ($0 < n < 27$)]: their unit cells contain 96 tetrahedral units with Si or Al as central atoms and oxygen as corner atoms. These structures (MFI; mordenite framework inverted) contain straight channels and zigzag channels, both with free apertures of about 0.55 nm in diameter. In general, self-diffusion coefficients decrease with increasing carbon number, are faster by a factor of 4-5

for zeolites without a counterion such as Na, and tend to be faster than comparable systems interrogated by pulse-field gradient NMR. In all probability, this discrepancy can be attributed to defects in the silicalite-1 structure. PFG-NMR, which measures displacements on the order of micrometers, is much more sensitive to such defects than QENS, which has an effective length scale of nanometers. Molecular simulations, which postulate a perfect crystalline structure, are closer to QENS than to PFG-NMR. For linear pores less than 1 nm in diameter there is a general tendency for the diffusion coefficients to decrease with increasing alkane chain length (Jobic et al 2010). This unexpected result (Fig. 10) can be explained by the fact *n*-butane keeps the same orientation in the 1D channels of the V⁴⁺-metal organic framework (MIL-47) so that it loses less momentum than propane, which tumbles within the pore channel.

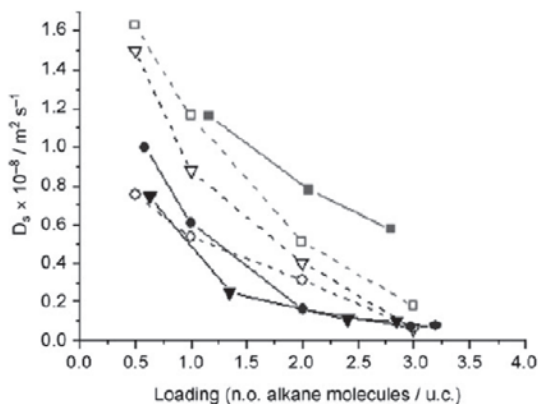


Figure 10. Self-diffusion coefficients (D_s) for ethane (square), propane (inverted triangle) and *n*-butane (circle) in V⁴⁺ MIL-47 metal organic framework as a function of the loading at 300 K. QENS (solid symbols), MD (open symbols). Note that the reported D_s values are orientationally averaged. [Used by permission of Wiley-VCH © 2010, from Jobic et al. (2010) *Chem Eur J*, Vol.16, Fig. 5, p. 10340.]

The properties of organic molecules in hydrated 2:1 clays have been studied by Skipper et al. (2006), who used QENS to show that methane interacts strongly with the clay, snugly fitting into the hexagonal ring sites on the clay surface, thus leading to a decrease of the diffusion coefficient by one order of magnitude as compared to bulk water-methane. Chathoth et al. (2010) presented results from a SNS-QENS study of the behavior of methane in a mesoporous carbon aerogel; a proxy for coal. The QENS portion of this study focused on the pressure and surface hydration effects on methane mobility. They observed a slowing of the motion for hydrated carbon pore walls compared to a “dry” carbon matrix. The pressure effect was non-linear with a subtle, yet measurable, maximum observed between ~3-4 MPa (maximum interrogated pressure was ~9 MPa). For the most part these various experiments were carried out at cryogenic to ambient temperatures and modest pressures, up to ~10 MPa.

NMR probes of hydrocarbons in nanopores

Diffusion considered as random motion of the elementary components of matter is among the most fundamental concepts in nature (Heitjans and Kärger 2005). This conceptual model is correct in the case of nanoporous systems as well. For this reason, studies of molecular diffusion in nanoporous materials attracted large interest. Among different techniques, pulsed field gradient (PFG) NMR has been proven to be very useful method to investigate systems with small molecules confined into the “subsurfaces” of nanoporous hosts (e.g., Meresi et al. 2001; Seland et al. 2001; Stallmach et al. 2000, 2001; Kärger et al. 2003; Krutyeva et al. 2007). PFG NMR diffusion measurements are based on pulse sequences forming a primary or stimulated spin echo of the magnetization of nuclei in resonance (Stallmach et al. 2000, 2001). In other words, the potential of PFG NMR depend on the amplitude and the rise and fall times of the

field gradient pulses (Kärger et al. 2003). Applying appropriate pulsed magnetic field gradients of duration δ , intensity g , and observation time t during the defocusing and refocusing cycles of the NMR pulse sequence leads to the spin echo being sensitive to the translational motion of the molecules (Stallmach et al. 2000, 2001). Depending on the measuring conditions, PFG NMR experiments on molecular diffusion in cavities of nanoporous host systems result in valuable information on different aspects of mass transfer. The valuable information covers 1) molecular diffusion in the interior particles; 2) hindered transportation by outer surface of particles; and 3) long-range diffusion. Thus, PFG NMR may yield the probability distribution $P(x,t)$ function that, during time t , a randomly selected molecule of the sample is shifted over a distance x in the direction of applied field gradient (Kärger 2008). Such capabilities of PFG NMR provides an opportunity to investigate diffusion behavior of molecules confined to both mesoporous and nanoporous systems (Stallmach et al. 2000, 2001; Kärger et al. 2003, 2009), to explore surface permeability of nanoporous particles (Krutyeva et al. 2007), to study transport properties of supercritical fluids in confined geometry (Dvoyashkin et al. 2007), and to study diffusion of small molecules such as methane and carbon dioxide in carbon molecular sieve membranes (Mueller et al. 2012). However, there are some problems in performing NMR experiments of diffusion of mixtures within porous materials since they represent heterogeneous systems (Pampel et al. 2005; Fernandez et al. 2008). In such heterogeneous systems, the transverse proton magnetization is decayed due to a continuous dipolar interaction between the spins of interest, as well as differences in the internal magnetic fields. These effects, including the restricted mobility of adsorbed molecules, broaden the NMR signal and results in reduced resolution (Pampel et al. 2005; Fernandez et al. 2008). The combination of PFG and MAS techniques overcomes this problem (Nivarthi et al. 1994; Pampel et al. 2003; Gaede et al. 2004). MAS PFG NMR enabled, for example, studying complex formation in an acetone-alkane mixture confined to nanoporous host systems (Fernandez et al. 2008) and molecular diffusion in zeolites (Pampel et al. 2005). A more interesting MAS probe without FG was designed to investigate the evolution of adsorption on nanoporous solids (see Fig. 11 by Xu et al. 2007). The results obtained by this technique depicted clearly the viability of a new technique for performing *in situ* solid-state NMR investigations of adsorption processes into nanoporous host systems and possible subsequent reactions. In addition to such PFG NMR and MAS PFG NMR studies on hydrocarbon derivatives confined into various host systems, there are recent attempts for studying such heterogeneous systems at low temperatures and high pressures (Huo et al. 2009; Hoyt et al. 2011).

One more potential method in analyzing small molecules in confined geometry is low-field (LF) NMR. LF-NMR has been used not only for the fast determination of the water and oil components in several food samples (Aeberhardt et al. 2007; Straadt et al. 2008), but also was applied for studying protein aggregation (Indrawati et al. 2007), detecting heterogeneities in polymer networks (Saalwachter 2003), and water diffusivity in aggregated systems (Guichet et al. 2008). LF-NMR measures the response of ^1H protons after immersing the collection of nuclei into an external magnetic field. Then the protons inside the sample

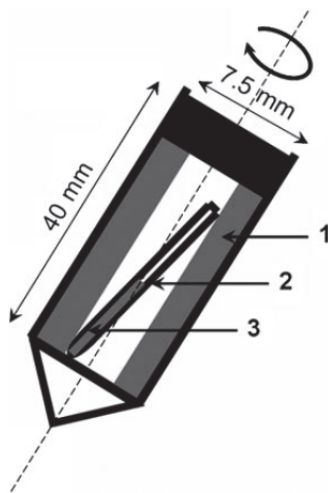


Figure 11. Schematic illustration of the setup for the *in situ* adsorption experiment inside the solid-state NMR rotor: 1) nanoporous material compacted on the walls of the rotor by prior spinning; 2) thin-walled glass capillary tube; 3) liquid to be adsorbed on the nanoporous material. [Used by permission of Wiley-VCH © 2007, from Xu et al. (2007) *Chem Phys Chem*, Vol. 8, Fig. 1, p. 1311.]

are polarized in the same direction with the external field. A radio-frequency field is applied to bring the protons to the perpendicular transverse plane. The magnetic signal processing in the transverse plane induces electric current, which is called the NMR signal or free induction decay (FID; Levitt 2001). The main advantage of LF-NMR experiments are based on time-domain relaxation measurements, such as transverse relaxation and longitudinal relaxation (no need to do Fourier transformed spectra analysis) and calibration of the instrument response or model-dependent analyses of the relaxation functions (Saalwachter 2003; Kantzas et al. 2005; Indrawati et al. 2007). The other benefits of LF-NMR technique are very short experimental time, very little if any sample preparation is necessary, and being non-destructive and non-invasive (Indrawati et al. 2007). In addition to relaxation measurements by LF-NMR, water diffusion coefficients in complex food products by low-field ^1H PFG-NMR were determined with standard errors lower than 0.5 % (Metais and Mariette 2003). Similar to this low-field, bench-top PFG NMR study on water diffusion in food products, Blümich et al. (2009) mentioned 2D relaxation exchange NMR of water in contact with nanoporous silica particles measured by low-field NMR. It seems that various NMR techniques ranging from low-field PFG NMR to high-pressure MAS NMR will contribute positively to the understanding of small molecule behaviors in confined geometry of subsurfaces.

Representative NMR studies

NMR studies of various hydrocarbons in nanoporous materials (mostly zeolites) are too voluminous to do justice to in this chapter, rather we will highlight some key results that illustrate the kinds of dynamical behavior hydrocarbons exhibit under nanoconfinement. Collectively these studies provide quantitative insights into hydrocarbon behavior as a function of particle size (i.e., transport length), pore diameter, pore geometry and pore intersection dimensions, cation size, ratio of Si:Al, hydrophobicity of the pore wall, load rate (i.e., amount of hydrocarbon), and hydrocarbon chain length.

Stallmach et al. (2001) demonstrated that PFG NMR can monitor anisotropic diffusion of slowly moving sorbate molecules arising from the inherent anisotropy of the MCM-41 nanopore system. As shown in Figure 12, there is significant deviation in non-exponentially decaying

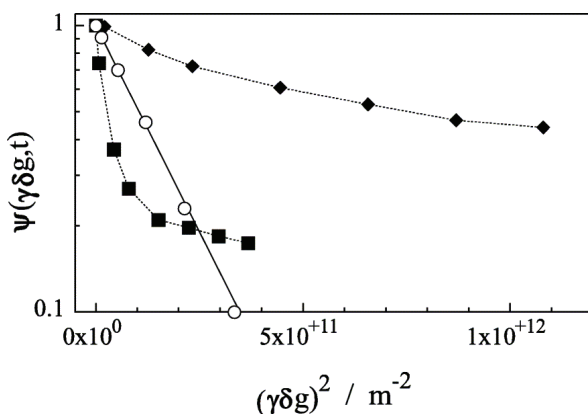


Figure 12. Examples for experimentally observed non-exponentially decaying PFG NMR spin echo intensities for benzene in two MCM-41 species (full symbols) compared with the exponential decay in the bulk liquid (open symbols) under the same conditions ($T = 298\text{ K}$, $t = 3\text{ ms}$). (◆) MCM-41 having particle size between 1 and 10 μm and pore radius 1.5 nm (■) Si-MCM-41 having particle size smaller than 1 μm and pore radius between 1.5 and 1.7 nm. [Used by permission of Elsevier © 2001, from Stallmach et al. (2001) *Microporous and Mesoporous Materials*, Vol. 44, Fig. 2, p. 750.]

PFG NMR spin echo intensities for benzene in two MCM-41 nanoporous hosts with respect to exponential decay in bulk benzene under the same experimental conditions. For instance, in sample MCM-41 the benzene exhibits slower decay than the bulk liquid, while in the case of Si-MCM-41 there is faster motion than the benzene in bulk.

Another host system of interest, zeolite NaX, has been studied by Kärger et al. (2003) with a mixture of *n*-butane and benzene. The zeolite hosts 0.8 molecules per supercage for *n*-butane and 2 molecules per supercage for benzene. The mobility of ethane in the nano-volume of zeolite NaX was also measured by PFG NMR. Figure 13 depicts temperature dependence of the coefficients of long-range diffusion of ethane upon confining into beds of zeolite NaX for two different loadings (Geier et al. 2002). The lower-temperature exponential dependence shifts to a much weaker dependence for higher temperatures. This change reflects the transition from Knudsen diffusion to bulk diffusion.

In a recent study by Dvoyashkin et al. (2007) using Vycor pore glass particles of about 500- μm size with mesoporous structure inside and 6-nm pore diameter, it was shown that a sufficiently large size of porous particles prevented extensive exchange between the bulk and the mesopores within the observation time $t = 3$ ms of the T_2 Hahn-echo pulse sequence (Figs. 14a,b). Both diffusivities D_b and D_p , in the bulk liquid and in the mesopores, respectively, increase at high temperatures following an Arrhenius law (the difference in absolute values attributed to the tortuosity of the porous space). Around 438 K an important deviation from the Arrhenius pattern in D_p was observed. However, at that temperature the diffusivity of the bulk liquid for the sample with Vycor did not exhibit noteworthy deviation from normal behavior.

One of the other NMR techniques employed in analyzing confined molecules behaviors was MAS PFG NMR. Fernandez et al. (2008) studied complex formation in acetone—*n*-alkanes (including hexane, heptane, and octane) mixtures by MAS PFG NMR diffusion measurements in two different specimens of trimethyl-silylized nanoporous silica gel. The silica gel nanoporous systems were synthesized from tetraethyl orthosilicate and had average pore sizes of 4 and 10 nm. MAS ^1H NMR was applied in order to resolve the signals of the acetone and the alkane constituent of interest. Upon resolving the signals of the two mixture components, comparing the CH_3 signals of acetone and the *n*-alkanes molecule yielded the acetone to *n*-alkane ratio. Selective diffusion measurements of acetone—*n*-alkane mixtures in both narrow (4 nm) and large

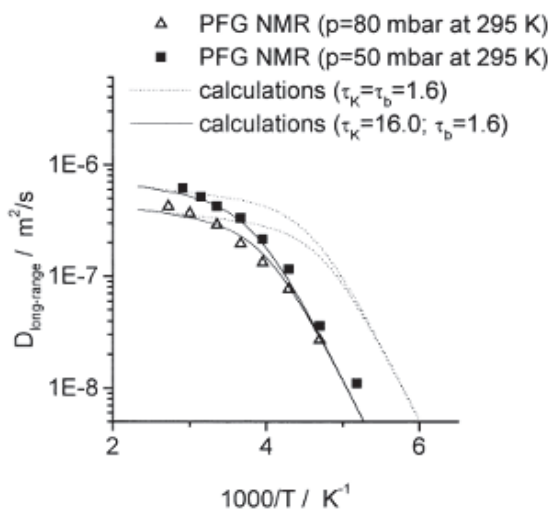


Figure 13. Temperature dependence of the coefficients of long-range diffusion of ethane measured by the PFG NMR method in beds of zeolite NaX for two different loadings (shown by the two different adsorbate pressures inside the sample tube at 295 K), comparison with the diffusivities calculated for identical and different tortuosity factors $\tau_{k(b)}$ in the cases of Knudsen and bulk diffusion using a simple kinetic gas approach. [Used by permission of American Institute of Physics © 2002, from Geier et al. (2002) *J Chem Phys*, Vol. 117, Fig. 1, p. 1936.]

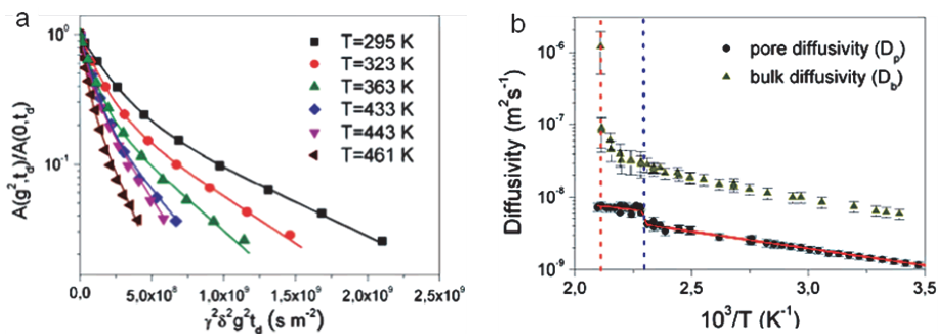


Figure 14. (a) Normalized spin-echo attenuation functions for *n*-pentane in Vycor porous glass obtained at different temperatures using PFG NMR. The solid lines show fits to the experimental data by two-exponential functions. (b) Arrhenius plot of the bulk and pore fluid diffusivities for *n*-pentane in Vycor porous glass. The solid line was calculated by assuming a transition to the supercritical state at $T = T_{cp}$. The vertical dashed lines show the positions of the bulk (left line) and pore (right line) critical points. [Used by permission of the American Chemical Society © 2007, from Dvoyashkin et al. (2007) *J Am Chem Soc*, Vol. 129, Fig. 1a, p. 10344-10345 (a), Fig. 1b, p. 10344-10345 (b).]

(10 nm) pore silica gels as a function of gradient amplitude at 298 K illustrated a notable deviation from a mono-exponential behavior observed in the free liquids. The deviation is stronger in the narrow-pore gel than in the large-pore one. This behavior was attributed to the deviation of the pore shapes (channel structure) from a cubic resulting in an orientation dependent anisotropic diffusion behavior. Additionally, examining the diffusion behavior of the two component mixtures in large and narrow pores indicated the following differences: 1) in large-pore gels the diffusivities increased by one or two orders of magnitude, 2) in large-pore gels the diffusion behavior difference of the *n*-alkanes and acetone disappeared, 3) in large-pore gels there is no longer any clear oscillation indication of the acetone diffusivities as a function of chain length of *n*-alkane molecules.

As mentioned in the introduction, Xu et al. (2007) developed a facile technique to handle MAS NMR for probing the adsorption of ^{13}C -labeled acetone on nanoporous MCM-41 and ZSM-5. MAS ^{13}C NMR spectra of acetone in MCM-41 pores acquired by spin rate of 3 kHz depicted that liquid acetone signals disappeared rapidly and were replaced by broader signals typical of acetone molecules in a less mobile environment (Fig. 15). Such a result indicates

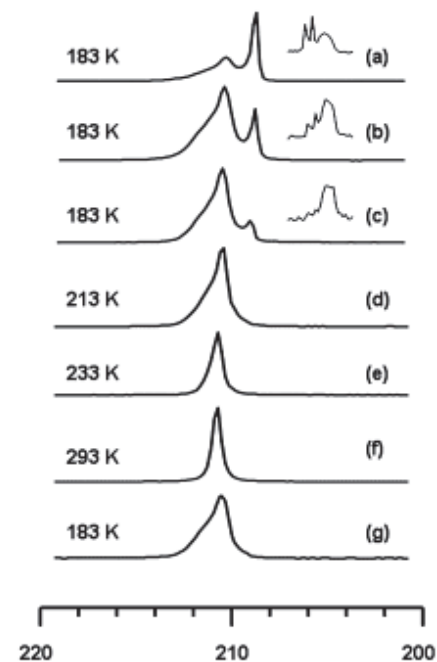


Figure 15. ^{13}C NMR spectra acquired as a function of time and temperature following adsorption of acetone on MCM-41, indicating the region of the spectrum for the (labeled) carbonyl carbon. In the spectra obtained at 183 K, the region corresponding to the (unlabeled) methyl carbon (between 27 and 32 ppm) is depicted as an inset. Each spectrum was acquired within 2 h. [Used by permission of Wiley-VCH © 2007, from Xu et al. (2007) *Chem Phys Chem*, Vol. 8, Fig. 2, p. 1311.]

that this technique may be provide a better understanding of adsorption processes into porous host systems.

Another study by Huo et al. (2009) employs MAS NMR on proton motion in confined geometry. Proton motion in HZSM-5, an acid catalyst widely used in petroleum industry, has been studied by low-temperature ^1H MAS NMR over the temperature range 150–295 K. The proton signal of the Brønsted acid sites ($-\text{OH}$) shifts to higher frequencies in the NMR spectra with decreasing temperature—a trend that is attributed to a gradual contraction of zeolite framework.

Another study reports a new high-pressure MAS NMR probe (Hoyt et al. 2011). Using this design, an internal pressure above 15 MPa was achieved without serious leakage problem during a time period of 72 h. The possible capability of this high-pressure MAS probe was demonstrated by carrying out *in situ* ^{13}C MAS NMR measurements of forsterite (Mg_2SiO_4) carbonation by mixture of supercritical CO_2 and H_2O at 15 MPa and 50 °C (Hoyt et al. 2011). The results indicate progressive carbonation reaction from solid phase reactants to solid-phase products—a result relevant to geological sequestration of carbon dioxide. This probe design will help scientists to investigate molecular interactions at the high temperatures and pressures expected in deep geologic reservoirs. Figure 16 summarizes *in situ* ^{13}C MAS NMR studies on Mg_2SiO_4 reacted with supercritical CO_2 and H_2O .

Quite often, NMR and QENS are used in concert with one another to quantify mobility of hydrocarbons in nanopores. For example, Jobic et al. (1995) determined the reasonably similar self-diffusivities of cyclohexane in microporous (pores < 2 nm) SiO_2 powder using both QENS and PFG-NMR. Since the time scale of the two methods are different; of the order of ms for PFG-NMR and ns for QENS, the mean-square displacements are of a different magnitude.

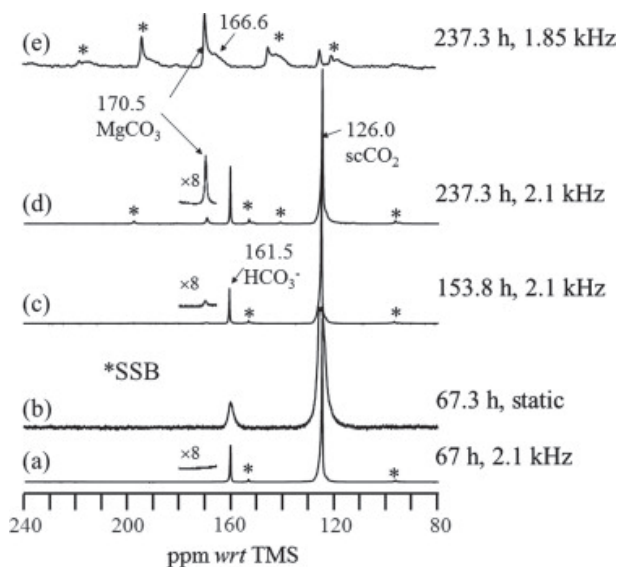


Figure 16. *In situ* ^{13}C single pulse MAS NMR spectra acquired at a spinning rate of 2.1 kHz on 0.27 g Mg_2SiO_4 + 0.1 g H_2O + 150 bar 14.3% ^{13}C enriched CO_2 + 1 g of extra H_2O separated from the forsterite powder at 50 °C for 67.3 h (including 17.3 h acquisition time) (a), 153.8 h (including 25 h second acquisition time period), (c) and 237.3 h (including 22 h third acquisition time period), respectively. (b) Static spectrum obtained immediately after (a). (e) MAS spectrum (d) and after the supercritical CO_2 was released. (*)s are spinning sidebands. The integrated peak area for the MgCO_3 , normalized to per unit number of accumulation increase by 6.4 fold from (c) to (d). [Used by permission of Elsevier © 2011, from Hoyt et al., (2011) *J Magn Res*, Vol. 212, Fig. 6, p. 383.]

They amount to several μm in PFG-NMR and to a few nm in QENS. The agreement between the two methods, within experimental error, indicates that the two techniques are measuring the same process; i.e., long-range translational motion. This result means that there are no dramatic transport resistances with spacing above the nm scale. The presence of transport resistance would lead to a reduction of the NMR diffusivities, while the QENS results would remain essentially unaffected by them (Jobic et al. 1995). At low loading (0.02 and 0.04 g cyclohexane per g SiO_2), the diffusion coefficients appear to be insensitive to the concentration, whereas at high loading, (0.08 g cyclohexane per g SiO_2) lower diffusivities are measured. Jobic et al. (1995) attribute this decrease in mobility to mutual hindrance of the molecules, which evidently becomes effective only at high concentrations. Activation energies of 10.9 and 11.6 kJ mol^{-1} were determined for lower loadings and the higher loading, respectively.

Another good example of the power of using combined ^2H -NMR and QENS was described by Stepanov et al. (2003) in a study of the translational and rotational dynamics of *n*-hexane in ZSM-5 and 5A zeolites (the characteristics of these are described above). There are profound differences between the two systems. In ZSM-5, the molecule sits in the channel segments and the energy barrier between two sites is small. On the other hand, in 5A zeolite, the molecule spends a longer time in the α -cages before jumping to the next cage. The ^2H -NMR spectra point out the more confined adsorption geometry of the molecule in the ZSM-5 structure, in the form of anisotropic motions, whereas isotropically reorienting molecules are evidenced in the α -cages of 5A zeolite. This result is in agreement with the larger entropy variations measured in silicalite (the Al-free analog of ZSM-5; Millot et al. 1998) compared with 0.5 nm zeolite (Paoli et al. 2002). Finally, the long-range diffusion coefficient of *n*-hexane, derived from neutron scattering techniques, is more than 4 orders of magnitude larger in ZSM-5, at 300 K, compared with 0.5 nm zeolite. This difference illustrates the drastic effect of the pore size and shape on the diffusivity of molecules in microporous materials. The reader should consult the excellent review articles on NMR studies of liquids in confined geometry by Packer (2003), Buntkowsky et al. (2007), and Webber (2010). For recent reviews of the application of neutron scattering and MD to both natural and engineered materials and their interaction with fluids see Cole et al. (2006, 2009, 2010).

ATOMIC AND MOLECULAR-LEVEL SIMULATIONS

Properties of confined fluids: do they differ compared to the bulk?

We briefly discuss herein effects on (1) the diffusivity of confined gas/liquids; (2) fluid adsorption and vapor-liquid equilibria for the confined fluids; and (3) liquid-solid transitions under confinement. These observations will be used in the section on “*Selected simulations of alkanes within alumina and silica-based pores,*” where we will discuss in a few more details the properties of confined alkanes. We provide a brief overview on simulation methods in the “*Simulation Details*” section.

Diffusion under confinement. The seminal works of Knudsen (1909), von Smoluchowski (1910), Pollard and Present (1948), and Mason et al. (1967) described confined fluid particles as hard spheres and took into consideration the momentum exchange between the fluid particles and the solid wall when the fluid-fluid interactions could be neglected, and later considered the effect of density on the mobility of the confined gases. More recently, theoretical developments have attempted to consider dispersive and longer-ranged fluid-fluid interactions (Guo et al. 2005, 2006). Building on the Chapman-Enskog kinetic theory approach (Davis 1992), Jepps et al. (2003) provided a significant improvement in our theoretical understanding of the diffusion of confined Lennard-Jones fluids by developing the “oscillator model” theory, which is exact at low confined fluid densities (i.e., low-pressure gases). The theory builds on the diffusive reflection model for fluid particles bouncing on the confining walls. To investigate the fluid

diffusion within pores of nano-scale dimensions (e.g., “nanopores”), theoretical investigations have benefited from advances in molecular simulation techniques. For example, recent simulation results suggest that, for fluids confined in carbon nanotubes, the specular reflection might be more accurate than the diffusive reflection model invoked in the groundbreaking theories discussed above (Skoulidas et al. 2002; Sokhan et al. 2002; Bhatia et al. 2005; Striolo 2006).

Bhatia and Nicholson (2007) recently extended the theories above to include the effect of loading (i.e., increased pressure). They compared the theoretical results to molecular simulation data, achieving satisfactory, though not quantitative agreement. In narrow cylindrical pores they showed that the diffusivity of confined methane is constant as the density increases (the simulations show slight increase), while in wider pores (albeit of diameter comparable to that of confined molecules) the diffusivity decreases as the density increases. In even larger pores it has been reported that the diffusivity increases as the density of the confined fluid increases because of viscoelastic effects (Bhatia and Nicholson 2006; Nguyen et al. 2006). In the case of alkanes adsorbed within silica mesopores at low loadings, it was observed by molecular dynamics simulations that the diffusivity of the alkane chains increases at the loading increases because of screened fluid-pore interactions (Raghavan and Macelroy 1995). Recent interest has been devoted to enhancing the permeability of natural gas through rock formations (e.g., shale deposits), as well as in sequestering carbon dioxide in geological formations. It has also been proposed to employ carbon dioxide as a fluid to enhance the permeability of natural gas, achieving simultaneously carbon dioxide sequestration and natural gas extraction. Clearly, for these applications to succeed it is necessary to understand how each of the gases diffuses in sub-micron, often nanometer scale pores. We summarize a few contributions to highlight extreme confinement effects.

Zeolites are among the most widely used porous materials in industrial applications. We refer here to the zeolite ZK5, which has a framework consisting of two different cages (the largest cavity, known as the α -cage, has diameter ~ 1.16 nm; the other cavity, the γ -cage, has cross section 0.66×1.08 nm) interconnected via circular rings of diameter 0.39 nm composed by 8 oxygen atoms (Zorine et al. 2004; Baerlocher et al. 2007). The size of both cages as well as that of the connecting ring is comparable to the molecular dimensions of alkane molecules such as *n*-pentane. At most, the unit cell of ZK5 can contain 12 *n*-pentane molecules, 3 in each of the α -cages, and 1 in each of the γ -cages. The question of interest here is how fast *n*-pentane molecules can diffuse across the zeolite. Experimental data have been obtained by ^{13}C NMR techniques when the zeolite was filled with *n*-pentane (Magusin et al. 1999). The results are consistent with a “hopping” diffusion mechanism with molecules jumping between neighboring cages with a hopping rate of 1 to 10^3 jumps per second in the temperature range 247 to 317 K. The resultant self-diffusion coefficient was found to be of the order 10^{-18} to 10^{-15} m^2/s .

Because of the extremely long time that separates distinct hopping events traditional “brute force” molecular dynamics simulation techniques cannot yield satisfactory information regarding this phenomenon. Alternative approaches have been designed. Saengsawang et al. (2010) applied the “high-temperature configuration-space exploration (HTCE)” method of Schuring et al. (2007) to overcome the limitations of standard molecular dynamics. In short, the rare-event hopping event of one *n*-pentane molecule from one α -cage to another was investigated at extremely high temperature (i.e., 6000 K), which makes the event more likely to be observed, and the results were appropriately corrected to become applicable in the temperature range of experimental interest. The transition state theory was then applied to obtain self-diffusion coefficients from the relative probability of observing the *n*-pentane molecules either within the cages, or inside the connecting oxygen rings. The self-diffusion coefficients obtained show Arrhenius dependence as a function of temperature, in general agreement with experiments. In Figure 17 we report a schematic for the ZK5 zeolite, the two cages occupied by *n*-pentane to

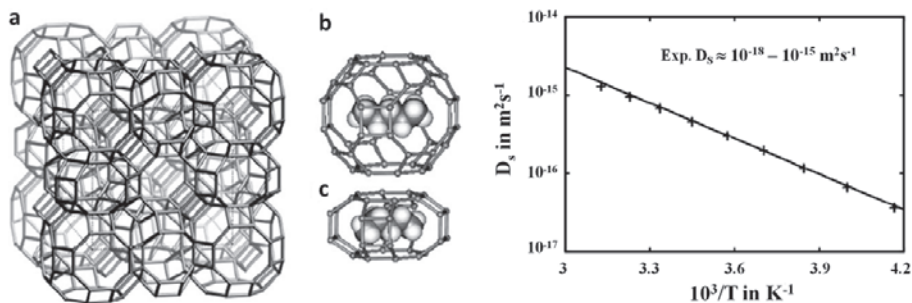


Figure 17. (left) Schematic representation of the ZK5 zeolite. Silicon or aluminum atoms constitute the vertices of the structure in panel (a). The various cages and how they are interconnected are visible from the schematic. Panels (b) and (c) show one *n*-pentane molecule inside α - and γ -cage, respectively. (right) predicted self-diffusion coefficients as a function of temperature. The predictions are in relatively good agreement with experiments. [Used by permission of Elsevier © 2010, from Saengsawang et al. (2010) *Chem Phys*, Vol. 368, Fig. 1, p. 122 and Fig. 5, p. 125.]

illustrate the level of confinement considered, and the self-diffusion coefficients predicted as a function of T . Although some differences do exist between experimental and simulated results (in part due to the different *n*-pentane loadings considered), this example shows how advanced simulations can elucidate the mechanism of diffusion for fluid molecules within extremely narrow porous networks.

To prevent, and when necessary remediate, environmental and energy challenges, it has been proposed to store CO_2 in deep un-minable coal beds, with the possible additional advantage of extracting trapped natural gas in the process (Busch et al. 2004; White et al. 2005). For such an application to be practically realized it is important to understand, quantify, and predict several physical-chemical aspects, including the adsorption and diffusion of both CH_4 and CO_2 within typical coal bed porous networks. Molecular dynamics simulations are being used for such purposes (i.e., to identify the relative diffusion and adsorption propensity of the two gases in the carbon-based pores; Hu et al. 2010). Firouzi and Wilcox (2012) employed the dual control volume grand canonical molecular dynamics algorithm (Heffelfinger and Van Swol 1994; Cracknell et al. 1995; Ford and Glandt 1995) to investigate the flux of pure methane, pure CO_2 , and their mixtures across representations of the carbon-based porous networks. The porous materials were obtained by implementing a geometric algorithm and the resultant models were characterized in terms of overall porosity and pore size distribution. Although some simplifications were necessary, the porous networks reproduced important experimental properties. Because of the large computational requirements, the fluid molecules were treated as spherical particles and all interactions were described by pair-wise Lennard-Jones potentials. One simulated system is reproduced in Figure 18, where an equimolar mixture of CH_4 (squares) and CO_2 (circles) are present in the two bulk reservoirs (left and right), and in the porous network (middle). The carbon atoms of the coal bed are not shown for clarity. The image represents pictorially the flux of both gases from the high-pressure region on the left (5 MPa) to the low pressure region on the right (2 MPa), and the presence of regions within the porous network that are not accessible to the fluid molecules, presumably because of the small pore size or because of lack of pore connectivity (the porosity of the material is 25% and the average pore size is 1.25 nm). Simulations were conducted as a function of the feed composition, the porosity of the substrate, and the difference in pressure between the two reservoirs. The results were quantified in terms of the permeability of the various gases. In the right panel of Figure 18 we reproduce simulation results for the permeability of the two gases in the mixture as a

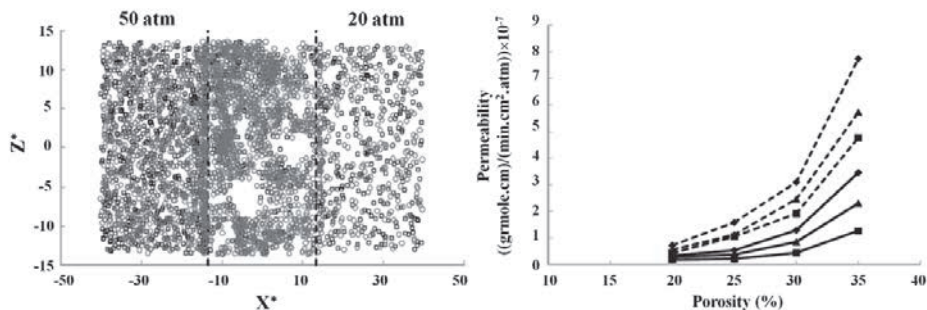


Figure 18. (left) Schematic representation of the system simulated by Firouzi and Wilcox to study the permeability of CH_4 - CO_2 mixtures across model coal beds. Squares and circles are for CH_4 and CO_2 molecules, respectively. The carbon atoms in the porous network are not shown for clarity. (right) Permeability of CH_4 (continuous lines) and CO_2 (dashed lines) through carbon-based porous materials with average pore size 1.25 nm and varying porosity. Different symbols are for varying methane mole fraction in the feed: diamonds, triangles, and squares are for 0.75, 0.5, and 0.25 CH_4 mole fraction, respectively. [Used by permission of Elsevier © 2012, from Firouzi and Wilcox (2012) *Microporous and Mesoporous Materials*, Vol. 158, Fig. 7, p. 201 and Fig. 10, p. 201.]

function of total porosity. The average pore size in all cases was 1.25 nm. As expected, the permeability increases with porosity. Important is that no detectable permeability was reported at porosity lower than $\sim 20\%$ because of the lack of connectivity between the pores. Simulations were conducted at varying methane mole fractions in the feed. The interesting observation is that both CH_4 and CO_2 permeability increase as the CH_4 mole fraction in the feed increases. Fully understanding the molecular reasons for these observations will certainly enhance the possibility of sequestering CO_2 in coal beds.

The simulations discussed above contrast a number of simulations available in the literature in which the adsorption and the diffusion of various gases were considered in simple pores, varying, for example, the pore width. Restricting our analysis to the case of carbon dioxide and methane, the recent reports by Lim and coworkers appear to be important. For example, Lim et al. (2010) simulated the adsorption of carbon dioxide (simulated using two different models, one spherical, the other, more realistic, linear) in carbon slit pores of various widths. The simulations were conducted at various bulk pressures and at various temperatures. The simulated diffusions were found to be much larger compared to experimental measurements, and were interpreted invoking a modified Knudsen diffusion mechanism. The authors suggest that the predicted values could be the upper limit available, when membranes could be prepared with perfect carbon pores as long as pore-entrance and pore-exit effects can be neglected. Lim and Bhatia (2011) extended the study to methane, and found that in the temperature range 298–318 K, and pressure range from 0.001 to 8 MPa, the permeability of methane in pores of width 0.65–0.75 nm is controlled more by the adsorption of the gas within the pores than by the self-diffusion coefficient.

When simulation results in individual pores, such as those just summarized, are available for individual gases and their mixtures, and when the resistance for the various gases to enter/exit the various pores are known, it will be possible to predict the permeability across realistic materials by implementing pore network models such as the one presented by Seaton and coworkers for the diffusion in nanoporous carbons (Cai et al. 2008). The validation of such models could be done by comparing the predicted permeability to simulated ones, such as those presented by Firouzi and Wilcox (2012), provided that the same porous network is used in both approaches.

Regarding the diffusion of trace elements (e.g., heavy metal ions) confined within narrow pores, we point out the work of Ho et al. (2012). These authors employed brute force equilibrium molecular dynamics simulations to quantify the mobility of aqueous NaCl or CsCl within slit-shaped silica-based pores of size ~ 1 nm. These simulations face several challenges, including the long time required to achieve equilibrium, the uncertainty regarding the composition of the confined system, and the slow dynamics typical of aqueous solutions under confinement. Despite these problems, the enormous computational resources that have become available to researchers have allowed Ho et al. (2012) to estimate the mobility of the various ions as a function of the degree of protonation of the confining surfaces. In Figure 19 we report a schematic of the system simulated, together with predicted planar self-diffusion coefficients, and the density distributions across the pore width for the various confined molecules. The results have been interpreted based on the expectation that water molecules diffuse slowly near a silica-based substrate (Argyris et al. 2009). As the degree of protonation changes, the preferential distribution of the various electrolytes across the pore width changes. Those ions that are preferentially found near the pore center have higher mobility than those that are preferentially found near the solid substrate. Such observations, if verified experimentally, could be useful for predicting the environmental fate of heavy metal ions accidentally released during operations such as mining.

Adsorption and vapor-liquid equilibria under confinement. Gelb and Gubbins provided an extensive review on the extent to which confinement leads to significant deviations for fluid thermodynamics properties compared to bulk (Gelb et al. 1999). One such effect is on the vapor-liquid coexistence curve (Striolo et al. 2005). A Monte Carlo study by Singh et al. (2009) elucidated the phase behavior of methane, butane, and other short alkanes confined in narrow slit-shaped carbon and mica pores. The results showed that as the pore width decreases the critical temperature decreases. Representative results are shown in Figure 20 for butane in mica and in carbon-based pores. Confinement was found to have a strong effect on the densities of the coexisting phases, and it was also found that the vapor-liquid surface tension for the confined alkanes is significantly reduced compared to values obtained in the bulk, possibly a direct consequence of the lower critical temperature for confined fluids.

As in the case of diffusion, the simulation studies that are being conducted for adsorption and phase transitions of various fluids in porous materials will help the interpretation of experimental data, as well as better understanding the behavior of fluids in subsurface conditions. However, to be useful the simulations need to be conducted carefully. For example, it is often tempting to employ simplified representations for the confining material. Smooth surfaces and simple geometries (e.g., cylindrical and slit shaped) lead to enormous savings of computational resources. However, details on the porous wall structure can lead to significant changes in the simulated adsorption isotherms (used to obtain results such as those in Figure 20, but also to predict the permeability of various gases). The simulation community is striving to generate computer models for the solid adsorbent that are more and more realistic. The literature is vast and not summarized here for the sake of brevity. Instead, we highlight a contribution from Coasne et al. (2006), who simulated the adsorption of simple Lennard-Jones gases in two models of the silica-based porous material MCM-41. One model had atomically smooth pore walls, the other was rough at the atomic scale. The adsorption isotherms obtained showed large adsorption-desorption hysteresis loops in the case of the smooth pore, and more gradual adsorption curves in the case of the rough surface. Careful analysis suggested that the smooth model yields results in agreement with experiments at short length, but not at large scales, while the rough model reproduces the surface disorder at large length scales but does not at short length scales. When the structure of the confined fluid is considered at those relative pressures at which the pores are not completely filled, the simulation results are dramatically different, as shown in Figure 21. Within the smooth pore (left panel) a clear separation is observed between

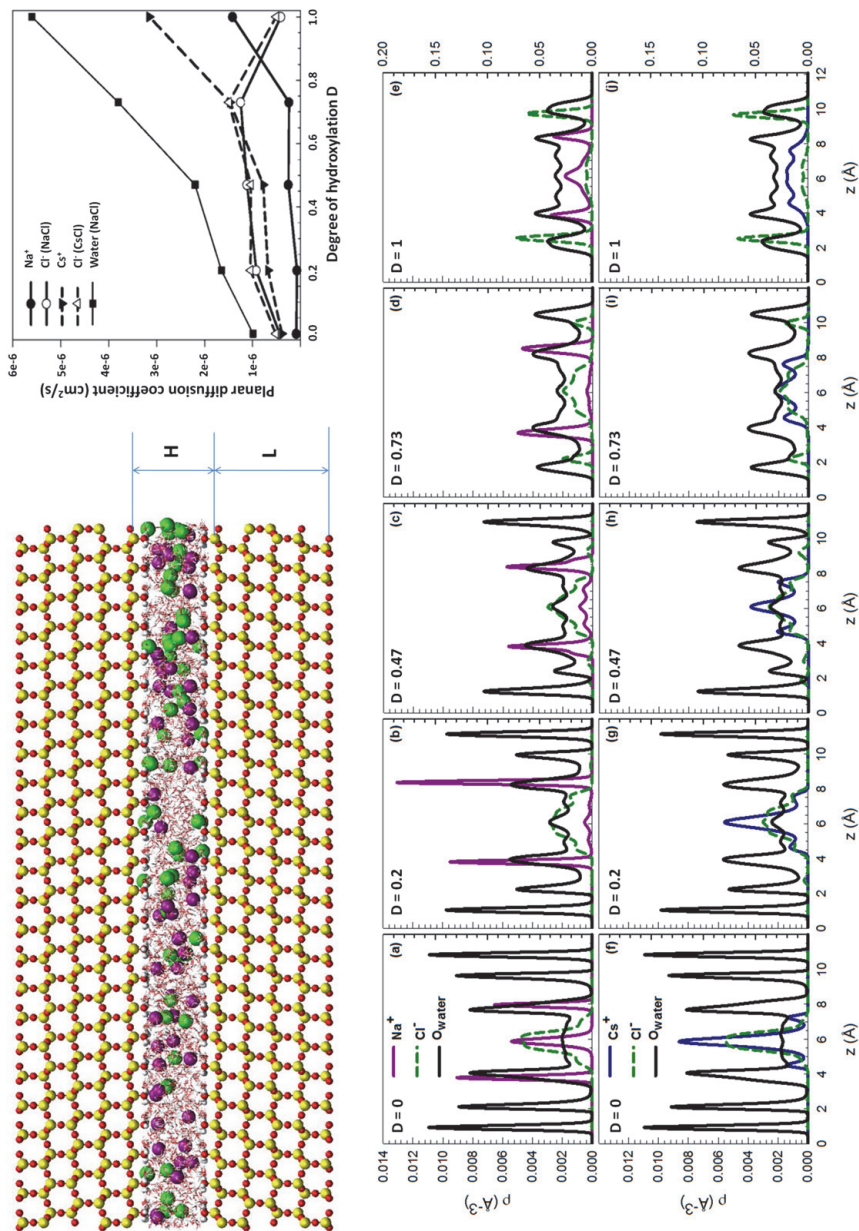


Figure 19. (top left) Schematic representation of the slit-shaped silica pores simulated by Ho et al. (2012). The pore width, H , is ~ 1 nm. (top right) Predicted in-plane self-diffusion coefficients for water and electrolytes within the pores as a function of the degree of protonation D . (bottom) Density distribution across the pore volume for oxygen atoms of water (dashed lines), Na⁺ (purple), Cs⁺ (blue), and Cl⁻ ions (dashed green lines) as a function of D . [Used by permission of the American Chemical Society © 2012, from Ho et al. (2012) *Langmuir*, Vol. 28, Fig. 1, p. 1257, Fig. 5, p. 1261, and Fig. 4, p. 1259.]

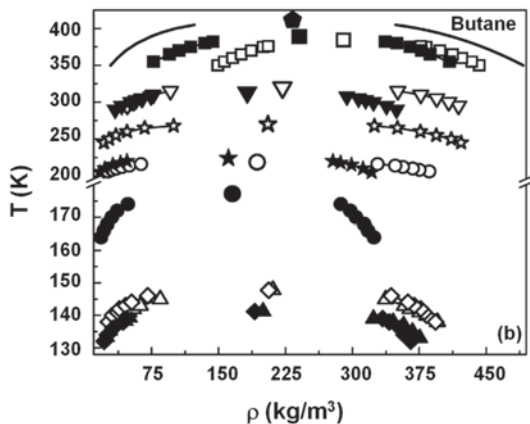


Figure 20. Vapor-liquid coexisting curves for butane confined in mica and graphite slit-shaped pores. The line represents the phase diagram in the bulk. Filled symbols are for graphite, open ones for mica pores. Different symbols are for pores of different widths. As the pore width decreases, the critical temperature decreases. [Used by permission of the American Chemical Society © 2009, from Singh et al. (2012) *J Phys Chem-C* Vol. 113, Fig. 2, p.7173.]

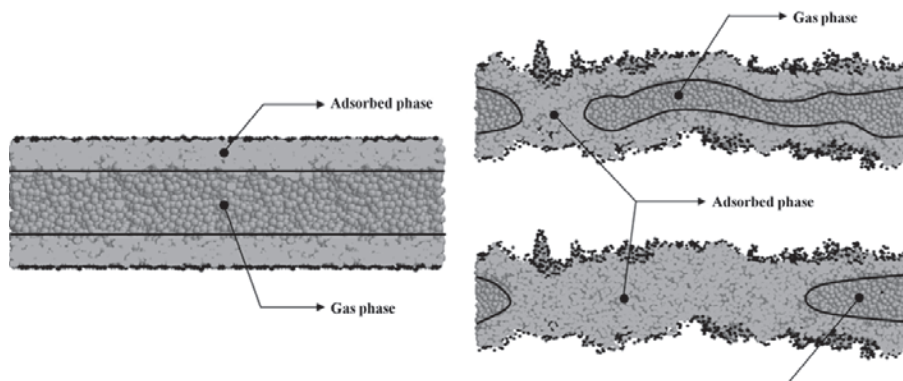


Figure 21. (left) Transverse section of a simulation snapshot illustrating Ar atoms adsorbed within a smooth model of the MCM-41 pore at 87K and relative pressure 0.69. The black lines divide the adsorbed fluid from the gaseous phase within the pore. (right) Transverse section of an atomically rough model pore partially filled with Ar at 87 K and relative pressures 0.44 (top) and 0.46 (bottom). Although the relative pressure is lower, the snapshots on the right suggest that the adsorbed phase fills more of the pore volume, and that the gaseous phase is trapped only within a few bubbles. [Used by permission of the American Chemical Society © 2006, from Coasne et al. (2006) *Langmuir*, Vol. 22, Fig. 7, p. 199 and Fig. 8, p. 200.]

the adsorbed fluid and the confined gas at the center of the pore, while in the rough pore model (right panel) a few bubbles of gas are found trapped within the adsorbed fluid. It is very likely that the transport properties in this dual-phase system strongly depend on the structure of the confined fluid, and therefore the predictions obtained with the two models are expected to be very different [no transport properties were reported by Coasne et al. (2006)]. Because subsurface pores are likely to be very heterogeneous in size, shape, surface morphology, and even chemical composition, in our opinion the observations from Coasne et al. (2006) should be kept in mind when simulation data are compared to experiments.

It is very likely that the phase equilibrium within the pores will determine the diffusion of confined substances. Ho et al. (2012), for example, found that aqueous Na^+ , Cs^+ , and Cl^- ions partition at different distances from the solid surface within the pores depending on the protonation state of the surface, leading to significantly different mobility for the various ions (see Fig. 19). Analogous results obtained for organic systems could lead to strategies for enhancing the

dislocation of various fluids trapped in subsurface formations. For example, the preferential adsorption of CO_2 compared to CH_4 near the carbon-based pores used in the simulations of Firouzi and Wilcox (2012) was invoked to explain the different permeability observed for the two gases, either pure or in binary mixtures (see Fig. 18). The preferential adsorption of CO_2 with respect to CH_4 in coal beds is the basis of the enhanced coal bed methane recovery (White et al. 2005). Unfortunately, this process is also responsible for the differential swelling of the coal (i.e., coal swells more when CO_2 is adsorbed than when CH_4 is adsorbed), which causes a reduced permeability of methane as CO_2 is injected. Brochard et al. (2012a) conducted a simulation study for the competitive adsorption of CO_2 and CH_4 in realistic models of carbon pores obtained with the reverse Monte Carlo method (Jain et al. 2006a,b; Nguyen et al. 2008). They considered temperatures and pressures representative for geological applications. They then applied a poromechanical model, developed independently by Brochard et al. (2012b), for predicting the material swelling as a function of the amount adsorbed. Representative results, shown in Figure 22, show that CO_2 adsorption is highly selective compared to CH_4 adsorption. Differential swelling is almost insensitive to the geological temperatures and pressures considered, while it appears to be proportional to the CO_2 mole fraction in the pores. Although swelling of coal beds is certainly dependent on additional factors, including the stress imposed in the rock formation by the surroundings, these results could aid interpretation and prediction of experimental observables.

As another example to illustrate preferential distributions of different fluids at contact with a solid substrate, in Figure 23 we compare preliminary simulation snapshots obtained for pure ethanol (left) and for an ethanol-water mixture (right) on a free-standing (0001) $\alpha\text{-Al}_2\text{O}_3$ substrate at 298 K and 0.1 MPa. When ethanol is the only fluid present, the results suggest the formation of a dense adsorbed layer on the substrate. When a small amount of water is added to the system, water molecules dislocate the adsorbed ethanol, they form a dense hydration layer, and the ethanol molecules are segregated further from the surface. Because those molecules (either ethanol or water) found in proximity to the substrate tend to show low mobility, should results similar to those presented in Figure 23 be observed also within narrow pores it is likely that pure ethanol will have low permeability within alumina-based rock formations, and that the addition of small amounts of water could potentially allow for an increased ethanol mobility. It is also possible that if the pores are extremely narrow, water molecules would fill the pores and block ethanol molecules from permeating the rock formation. Clearly, careful verification of such predictions needs to be conducted. This brief discussion points out the need of carefully analyzing the composition of the subsurface fluids, together with details concerning the pore network (e.g., pore size, shape, entrance, and chemical composition) for predicting the permeability of different fluid systems.

Liquid-solid transitions under confinement. Using macroscopic thermodynamic arguments (equating the free energies of confined solid and liquid phases, Warnock et al. 1986), or calculating the chemical potential as a function of temperature for confined liquid and solid phases (Evans and Marconi 1987), it is possible to derive the Gibbs-Thomson equation to relate the freezing temperature for a confined fluid to the pore size. The latter relation is invoked in the experimental technique of thermoporometry, used to characterize porous materials (Eyraud et al. 1988). Unfortunately, the Gibbs-Thomson relationship fails as the pore size becomes comparable to the molecular diameter. Alba-Simionesco et al. (2006) provided a clear and concise review on the subject. Recent results show that the freezing temperature of the confined fluid can increase or decrease compared to bulk values, depending on whether the fluid-wall interactions are weaker or stronger than fluid-fluid interactions, respectively. Sometimes exotic phases, not observable for bulk systems, can be observed under confinement (e.g., the hexatic phase) (Radhakrishnan et al. 2000, 2002).

Combining experiments and simulations leads to important observations regarding the fluid-solid transition for confined systems. For example, Coasne et al. (2009) investigated, using

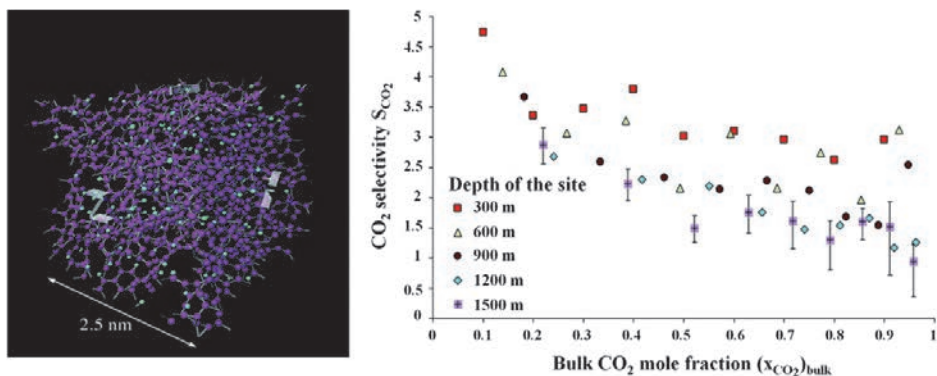


Figure 22. (left) Schematic representation of the model used to simulate a carbon adsorbent (i.e., coal bed). (right) Selectivity of CO₂ with respect to CH₄ adsorption as a function of bulk CO₂ mole fraction. Different symbols represent data obtained at different geological conditions (depths of the coal bed). Note that in most cases the selectivity is well above 1. [Used by permission of the American Chemical Society © 2012, from Brochard et al. (2012a) *Langmuir*, Vol. 22, Fig. 1, p. 2661 and Fig. 6, p. 2664.]

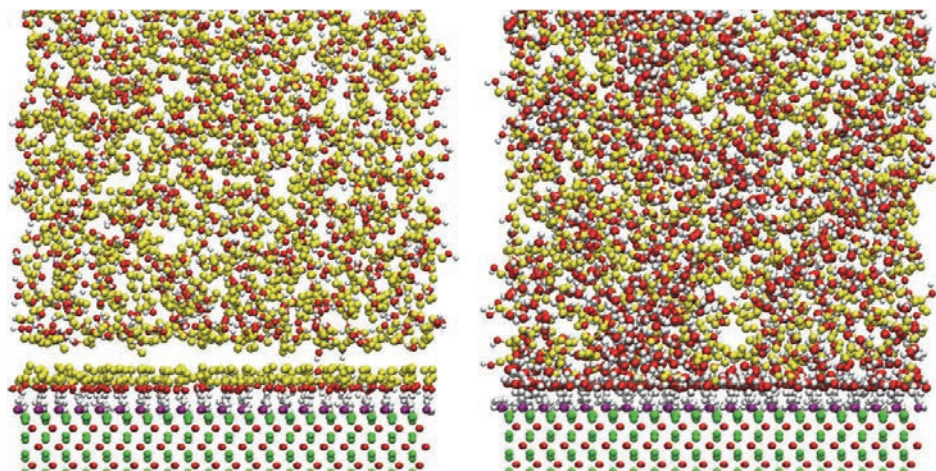


Figure 23. Preliminary simulation results for pure ethanol (left panel) and for a water-ethanol mixture containing 50% water molecules (right panel) at contact with a free-standing fully protonated (0001) α -Al₂O₃ surface. Ethanol molecules are shown in yellow (red and white are for the OH groups). Simulations performed at 298 K and 0.1 MPa. Note that when ethanol is at contact with the substrate, a dense layer forms near the surface. As water molecules are added to the system, these replace ethanol and form one dense hydration layer near the substrate. Because those fluid molecules near the substrate tend to show lower mobility than those far from it, these preliminary simulation results suggest that adding some water could enhance the permeability of ethanol through alumina-based rock formations.

parallel tempering Monte Carlo techniques, the freezing of pure methane and argon, as well as of their mixtures in a slit-shaped graphitic pore. Because the pore is strongly attractive to both fluids, the freezing temperature for both confined substances, as well as for their mixtures, was found to be larger than that in the bulk. The phase diagram for the confined mixture showed an azeotrope, similarly to that observed for the bulk mixture. Regarding azeotropic mixtures, Czwartos et al. (2005) reported dielectric spectroscopy experiments for CCl₄/C₆H₁₂ mixtures confined in carbon fibers and grand canonical Monte Carlo simulations for Ar/CH₄ mixtures

confined in carbon-slit pores. The results are summarized in Figure 24. Both experiments and simulations show that qualitatively the phase diagram for either mixture does not change upon confinement (note the azeotrope). However, because all fluids considered are strongly attracted to the confining pores, the coexistence lines are shifted to higher temperatures upon confinement. The other important observation is that the composition of the azeotrope is enriched in the component that is most strongly attracted to the carbon pores (C_6H_{12} in the case of the CCl_4/C_6H_{12} mixture, Ar in the case of the Ar/ CH_4 mixture). A cautionary note should be made here, as the experiments could not assess the composition of the mixture under confinement. The authors speculate that the experimental mole fractions for the confined system under-estimate the mole fraction of C_6H_{12} , as this substance is more strongly attracted to the carbon surfaces.

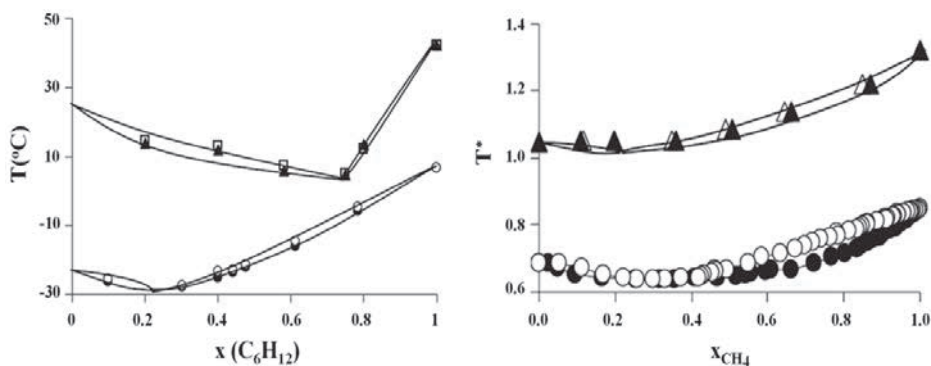


Figure 24. (left) Experimental phase diagram for CCl_4/C_6H_{12} mixtures (mole fraction) as measured by dielectric spectroscopy in activated carbon fibers. Circles are for the bulk mixtures, triangles and squares are for the mixtures at contact with the porous adsorbent. Because the experiments were conducted for fluid mixtures at contact with the porous material, the compositions reported are for the overall system. (right) Simulated phase diagram for Ar/ CH_4 mixtures in graphitic slit pores. Circles are for the bulk mixtures, triangles for the mixtures under confinement. In both panels open and closed symbols are liquid and solid coexistence data, respectively; lines are guides to the eye. [Used by permission of Taylor and Francis © 2005, from J. Czwartos et al. (2005) *Molecular Physics*, Vol. 103, Fig. 3, p. 3107 and Fig. 9, p. 3110.]

Given the interest in carbon-based pores for the possible combined application of CO_2 sequestration and enhanced methane recovery, it is worth highlighting some results reported by Hung et al. (2005). These authors conducted Monte Carlo simulation studies for Lennard-Jones fluids confined within carbon nanotubes. The results showed that the tube diameter is very important in determining not only the solid-liquid transition for the confined fluid, but also the structure of the solid phase under confinement. In particular, when the tube diameter was ~ 9.6 times the diameter of one fluid molecule the simulations did not show a solid structure similar to the one observed in the bulk. Further, while the molecules in contact with the confining walls showed an increase in the freezing temperature, those close to the nanotube center showed a depression in the freezing temperature. The simulation results appeared to be in reasonable agreement with dielectric spectroscopy experiments. There is no doubt that freezing will have a strong effect on the mobility of the confined fluids. It is possible that some fluid, maybe present in small amounts within the porous network, by freezing effectively blocks some pores and reduces the rock permeability. These effects could be facilitated by the strong expansions (from high to ambient pressures) typically observed when natural gas and/or other geological fluids are extracted from geological formations.

Selected simulations of alkanes within alumina and silica-based pores

Simulations, in particular molecular dynamics (complemented by Monte Carlo and *ab initio* density functional theory, DFT), have become a routine tool to study the properties of bulk fluids, including those of water, alkanes, and their mixtures. Unfortunately, studying fluids at contact with a solid substrate is hindered by the uncertainties regarding the solid-fluid interaction potentials, and also by the fact that the relaxation time of the solid is typically much longer than that of the fluid. However, it is now recognized that simulation results can significantly improve the interpretation of experimental data, especially when direct observation is difficult, as in the case of confined fluids. Some examples have been given in the “*Properties of confined fluid*” section. More and more evidence suggests that semi-quantitative agreement can be obtained between simulation predictions (sometimes even obtained by implementing force fields not necessarily derived to reproduce experimental data for fluid-solid interfaces) and experimental observations. When some disagreement is observed, it could be used as a valid reason to improve the simulation models, but also to revisit the interpretation of the experimental data, which could lead to discoveries. We highlight below a few simulation studies for alkanes in contact with alumina and porous silica. Compared to the studies for simple fluids, which have been the basis for the general aspects discussed above, the studies for long alkanes are somewhat limited. As the importance of understanding fluid behavior and rock-fluid interactions in subsurface formations grows, so is the need to further the investigations summarized herein.

Alkanes near alumina. Alumina is frequently used as catalyst and catalyst support, and it also constitutes part of clay, a naturally occurring material. Understanding the behavior of fluids near to, or confined between, alumina surfaces is therefore of wide interest.

The Al-terminated α -Al₂O₃ surface shows significant relaxation of the solid atoms, as suggested by both theoretical (Konstadinidis et al. 1992; Manassidis and Gillan 1994; Streitz and Mintmire 1994) and experimental observations (Ahn and Rabalais 1997). It also readily reacts when exposed to water. The hydroxylated form of the α -Al₂O₃ surface shows limited relaxation (Wittbrodt et al. 1998). Whether or not the solid atoms near the interface relax compared to the positions they would occupy in the bulk of the material has important consequences in the structure predicted for interfacial fluids. For example, Li and Choi (2007) employed a number of techniques to study linear C-11 and C-200 alkanes on an alumina support. They first relaxed the Al-terminated alumina substrate using *ab initio* DFT, and then used molecular dynamics (MD) to study the structure of the liquid alkanes adsorbed onto the substrate, maintained rigidly. Representative results, shown in Figure 25, are interesting for a number of reasons: (1) the density profiles obtained for the short alkane are qualitatively, though not quantitatively, similar to those obtained for the long chains, which is consistent with surface force apparatus (SFA) experiments for alkanes of different lengths confined between mica surfaces; and (2) the relaxed alumina substrate promotes the formation of well-defined density layers formed by alkane segments (CH₃ groups) as the distance from the surface increases while the non-relaxed surface does not (these observations suggest that the relaxed alumina support is commensurate with the alkane molecules and promotes the formation of contact layers within which the alkane chains lay parallel to the solid surface).

Jin et al. (2000) obtained results to some extent analogous to those just discussed when they employed MD to study the structure of C-8, C-16, and C-32 alkanes confined between two parallel alumina surfaces. The alumina surfaces were hydroxylated, and the authors reported limited relaxation compared to bulk structures when DFT calculations were performed (Wittbrodt et al. 1998). Thus, a crystalline structure was assumed for the solid. The simulations were conducted at 300 K. Pronounced layering was observed in the atomic density profiles for up to 4-5 atomic layers (up to 2.0-2.5 nm) from each surface. The density profiles were qualitatively similar for all alkanes considered. This result (layering) appears to be consistent

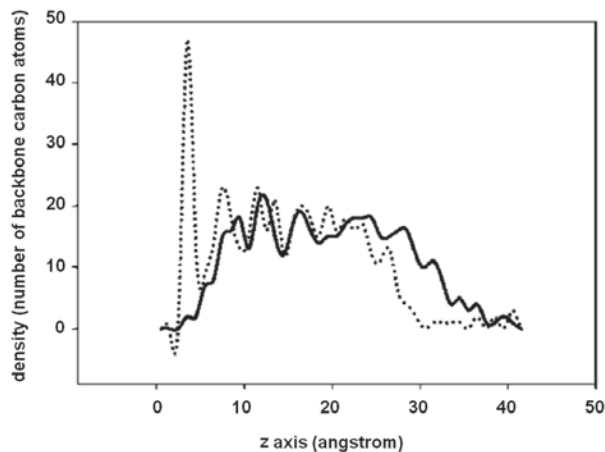


Figure 25. Density profiles for CH_2/CH_3 groups as a function of the distance from a flat alumina substrate. Results are shown before the substrate was relaxed (black line) and after the relaxation (dotted line). Relaxing the surface yields pronounced layering in the film. [Used by permission of the American Chemical Society © 2007, from Li and Choi (2007) *J Phys Chem-C*, Vol. 111, Fig. 4, p. 1751.]

with a number of simulation results for liquid straight-chain alkanes confined between two parallel surfaces (Bitsanis and Hadziioannou 1990; Vacatello et al. 1990; Balasubramanian et al. 1995, 1996; Dijkstra 1997; Gao et al. 1997a,b; Wang and Fichthorn 1998), structured or unstructured (Magda et al. 1985). Compared to results obtained by Li and Choi (2007), the simulations reported by Jin et al. (2000) were conducted for fluid molecules confined within two parallel surfaces, which in general promotes longer-ranged ordering than does one free-standing surface. This difference might be the reason why Li and Choi did not report ordering for alkanes adsorbed on a non-relaxed surfaces, whereas Jin et al. found pronounced ordering for any type of confining surfaces.

In addition, by analyzing the layer-by-layer intra-molecular radial distribution functions Jin et al. (2000) showed that the alkane chains adsorbed onto the alumina substrate have a tendency to adopt a trans conformation, which has also been found for alkanes adsorbed on gold (Balasubramanian et al. 1995). Finally, the dynamics of the adsorbed alkane chains were found to be significantly delayed compared to that of bulk alkanes, and infrequent exchanges were observed between alkanes belonging to different layers (the simulations were only conducted for at most 1 ns; current computational capabilities would allow researchers to reach up to 50-100 ns). This latter observation suggests the existence of a correlation between spatial distribution and dynamic properties. Namely, the alkane chains that are located near the surfaces show less mobility than those found away from the surfaces, suggesting that when a technology is designed to “detach” the alkanes from the pore surfaces, enhanced permeability could be achieved.

Along these lines, de Sainte Claire et al. (1997) conducted MD simulations for a system composed of a free-standing Al-terminated alumina surface, a thin layer of pre-adsorbed alkanes (butane, octane, and dodecane), and a small cluster of 30 water molecules. They found that the water molecules penetrate the pre-adsorbed thin film of alkane chains because they are attracted to the alumina substrate via long-range electrostatic interactions. During the penetration process, a competition was found between the displacement of the hydrocarbon chains, and the densification of the adsorbed thin film. Both phenomena were caused by the penetrating water molecules. The process of penetration was found to become more difficult as the alkane chain length increased and as the temperature decreased. In Figure 26 we reproduce the simulation results for the evolution of the probability of finding water molecules at various distances from the alumina substrate when the 30 water molecules were placed near the bare alumina (left) or near the alumina substrate covered by 2.6 monolayers of octane. In the case

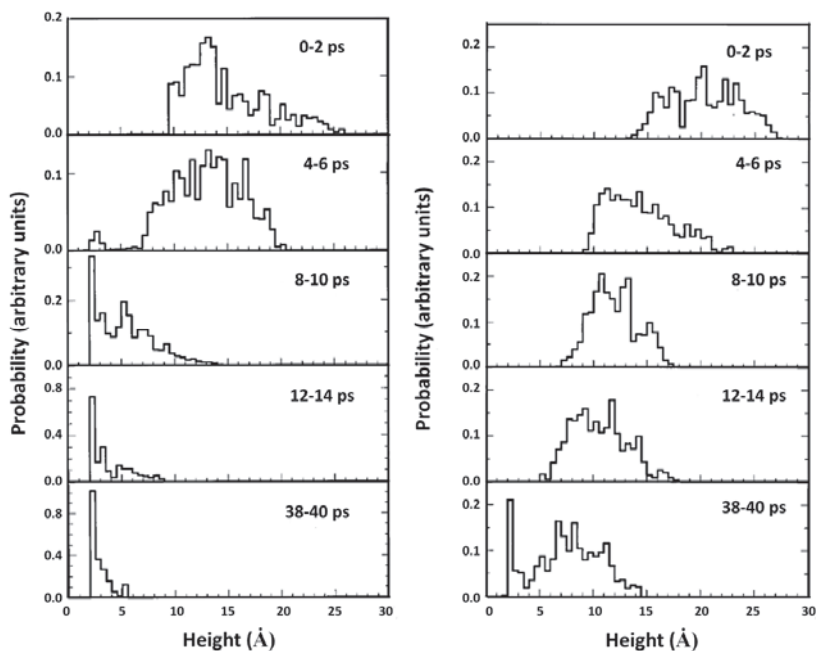


Figure 26. Time evolution of the density probability of observing water molecules at various vertical distances from the (0001) surface of α - Al_2O_3 . In the left panel a cluster of 30 water molecules was placed initially at about 1.5 nm from the bare surface. On the right panel the cluster of 30 water molecules was placed on a surface on which 2.6 monolayers of octane were pre-adsorbed. The time intervals indicate the length of the MD simulations performed. Water molecules quickly adsorb and spread on the bare surface, yielding a monolayer (*left*). When the surface is covered by octane (*right*) water molecules manage to come in contact with the alumina substrate, although a perfect monolayer is not obtained within the 40 ps of the simulations presented. Simulations were performed at 300 K. [Used by permission of American Institute of Physics © 1997, from de Sainte Claire et al. (1997) *J Chem Phys*, Vol. 106, Fig. 6, p. 7339 and, Fig. 9, p. 7340.]

of water on bare alumina, water molecules readily form a monolayer on the substrate, which is in qualitative agreement with recent MD simulations (Argyris et al. 2011). When octane is present the water molecules still manage to come in contact with the substrate, although the process takes longer to complete and the distribution of water molecules after 40 ps spans the ~ 1.5 nm near the substrate. Note that in recent years computational capabilities have become highly evolved, and it would now be possible to perform simulations such as those of Figure 26 for several hundreds of ns.

Studies such as the one just summarized are important for providing interpretation to detailed experimental studies of alkane-mineral interfaces, such as, for example, the broadband sum frequency generation studies recently reported by Buchbinder et al. (2010). Other simulation studies along similar lines have investigated the deposition of waxes on hematite (San-Miguel and Rodger 2003), sometimes in the presence of other compounds (San-Miguel and Rodger 2010).

Regarding confined mixtures, it should be pointed out that smectites, present in sediments and soil, have been found to host a variety of hydrated organic molecules in their interlayer (Kaiser and Guggenberger 2000; Kennedy et al. 2002; Kawahigashi et al. 2006), and that large amounts of methane appear to be stored in clay minerals present in marine sediments (Hinrichs et al. 2006; Ertefai et al. 2010). These observations stimulated experimental (Cha et al. 1988;

Guggenheim and Koster van Groos 2003; Seo et al. 2009) and simulation (Sposito et al. 1999; Titiloye and Skipper 2000; Park and Sposito 2003; Cygan et al. 2004a; Zhang and Choi 2006; Zhou et al. 2011) studies for methane-water mixtures confined within various smectites. The simulation results suggest that under confinement one methane molecule is hydrated by ~12-13 water molecules and remains at contact with ~6 oxygen atoms on the clay surface. Because in bulk hydrates one methane molecule is hydrated by 21 waters (Koh et al. 2000), the simulations suggest that methane prefers to accumulate near the solid substrate when it is confined in smectites.

When MD simulations are conducted to study mixtures, one source of uncertainty is whether or not the system studied is at equilibrium. At equilibrium the chemical potential for each of the fluid molecules under confinement should be equal to that of the fluid molecules in a correspondent bulk mixture. Typically, grand canonical Monte Carlo simulations are conducted to ensure that the chemical potential of a fluid under confinement is equal to that of the fluid in the bulk (Nicholson and Parsonage 1982). Indeed, by implementing such algorithms it is possible to simulate adsorption isotherms for various fluids, pure or mixtures, into porous materials. However, for dense systems composed of long hydrocarbons, and maybe containing hydrogen-bonding fluids under confinement, the acceptance of addition/deletion Monte Carlo moves is likely to be very low, and advanced simulation schemes need to be implemented. To overcome this requirement, and taking advantage of the enormous computational resources that are becoming available, we have implemented MD procedures to attempt to investigate the equilibrium partition of different fluid molecules between bulk systems and nanometer-scale pores. In Figure 27 we show one simulation snapshot, obtained for a mixture of water and methane at contact with a narrow slit-shaped Al_2O_3 pore of width ~1 nm. The alumina substrate is fully hydroxylated. Although the simulations are still preliminary, and proper assessment of their reliability has yet to be completed (e.g., we need to ensure that similar results are obtained when simulations are conducted from different initial configurations), the results clearly show that the bulk behavior of the water-methane mixture differs substantially compared to the behavior of the mixture under confinement. Water appears to be strongly attracted to the slit pore, while methane prefers to stay in the bulk region. A few water molecules escape the pore volume, but remain close to the pore entrance, where they can form energetically advantageous hydrogen bonds with other water molecules, and also interact favorably with the solid atoms. Although most methane molecules remain outside of the pore in the bulk, some methane molecules are found trapped within the pore. Contrary to what has been suggested in the case of smectites, the simulation snapshots of Figure 27 (see expanded view in the bottom panel) suggest that methane molecules prefer to accumulate near the pore center, where they are completely surrounded by water. Understanding how the structure of hydrated methane changes as the pore width and the pore chemistry change is important for a number of practical applications that include hydraulic fracturing. It appears that simulations, especially when synergistically coupled with experimental characterization, have the potential of helping this important quest.

Alkanes in silica-based porous materials. Many studies have focused on uncovering the properties of alkanes confined within silica-based pores. In particular, large attention has been given to zeolites, which are aluminosilicates. The composition of the zeolite has important consequences on its chemical physical properties. For example, when the aluminum content is high the zeolite is expected to become highly polar; as a consequence, preferential adsorption of polar molecules (e.g., water) is expected. Under such circumstances even small amounts of water present in the system can affect the adsorption of other gases (Brandani and Ruthven 2004; Galhotra et al. 2009; see, as a only partially related example, the simulation snapshot of Fig. 27). For example, the FAU type X zeolite, with a Si to Al ratio of 1-1.5, has been used in the form of membranes for the separation of methanol and water from systems containing hydrogen and carbon dioxide, respectively, in a large temperature interval (Sandstrom et al. 2010).

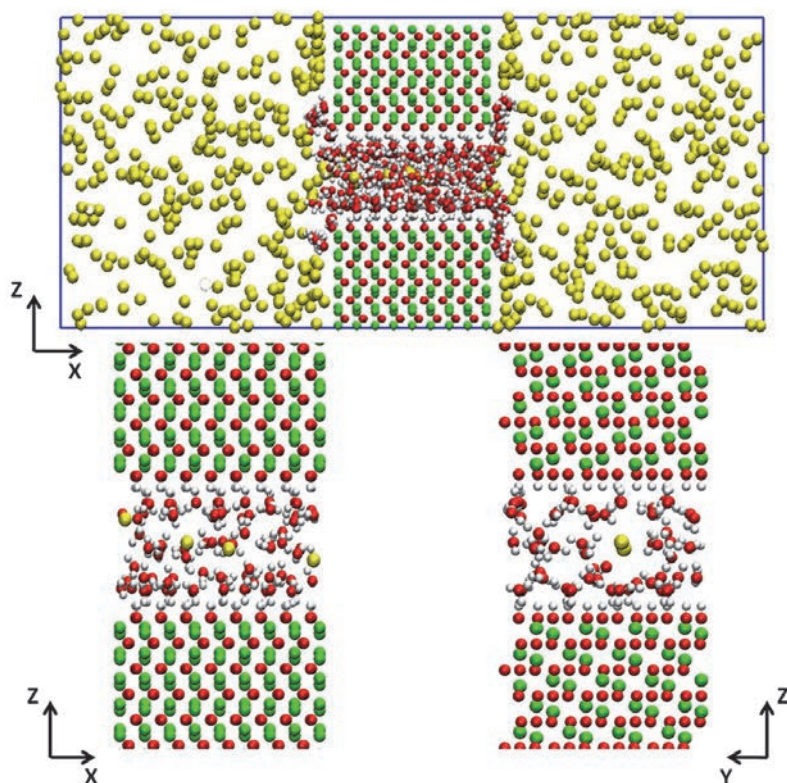


Figure 27. Preliminary simulation snapshot for a fluid system composed of methane (yellow spheres) and water molecules (red and white spheres represent oxygen and hydrogen atoms, respectively) partitioned between a bulk region (enriched in methane) and a slit-shaped pore of width ~ 1 nm. The pore is obtained by two facing surfaces of hydroxylated α - Al_2O_3 . The bottom panels are enlargements of the simulation snapshot in the top panel, showing how the methane molecules trapped within the pore are preferentially found near the pore center, surrounded by water molecules. Simulations were performed at 300 K and 8-10 MPa for a mixture containing 50% methane molecules.

Due to a number of practical applications not limited to extraction of hydrocarbons from subsurface formations (e.g., catalysis), the study of alkanes, as well as of their mixtures confined in zeolites is growing rapidly. In Figure 28 we reproduce high-resolution scanning transmission electron microscopy images for the HY zeolite recently reported by Lu et al. (2012). In this study iridium is deposited on the zeolite for catalytic purposes, which is beyond the scopes of this chapter. The figure is important for remembering the high degree of confinement expected for fluids confined within zeolites (see, for example, Fig. 17 for a discussion on this topic). Because of space limitations we concentrate primarily on pioneering recent contributions.

Smit pioneered the use of simulations, including Monte Carlo and MD, to understand the behavior of molecules confined within zeolites for explaining observations in catalysis. He studied simultaneously the effects of alkane adsorption within the zeolite pores, their diffusion, and their catalytic conversion. For example, Smit and Maesen (1995) employed grand canonical Monte Carlo simulations to study the adsorption of butane, hexane, and heptane in silicalite. They demonstrated that unexpected, and at the time still unexplained, features in experimental adsorption isotherms could be explained by a phase transition experienced by confined hexane and heptane molecules that lead to a collective freezing. The phase transition could only be

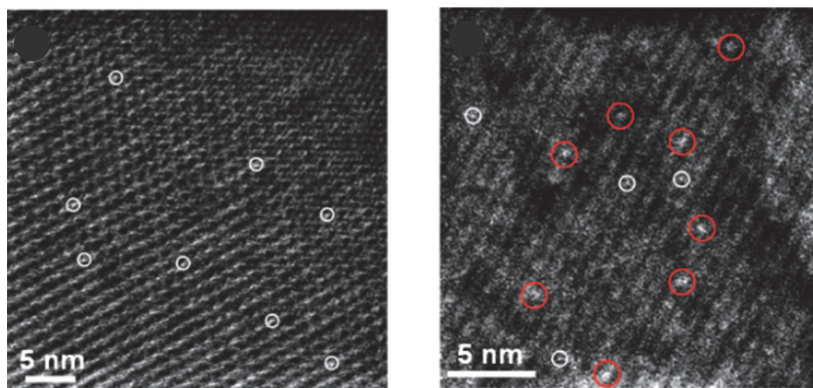


Figure 28. High resolution scanning transmission electron microscopy images of HY zeolite as prepared with Ir(C₂H₄), (*left*), and after 1 h of flowing H₂ at 300 K (*right*). The treatment causes individual Ir atoms (circled in white) to coalesce into clusters, circled in red. [Used by permission of the American Chemical Society © 2012, from Lu et al. (2012) *J Am Chem Soc*, Vol. 134, Fig. 1, p. 5022.]

observed for hexane and heptane because their length is commensurate with the porous structure of silicalite. For shorter and longer chains, similar phase transitions could not occur because of thermodynamic considerations, and typical type-I adsorption isotherms were obtained, both experimentally and by simulations. More recently adsorption isotherms have been calculated using Monte Carlo simulations by Ndjaka et al. (2004) for several short alkanes (methane, ethane, and propane) in a few different zeolites. The various zeolites selected are characterized by a relatively wide range of pore sizes, and the results, obtained implementing the Lennard-Jones parameters proposed by Vlugt et al. (1999), yield good comparison to experimental observations.

The diffusivity of methane, ethane, and propane was assessed via MD simulations within mordenite, zeolite EU-1, and silicalite (Nowak et al. 1991). The analysis of the simulation trajectories showed that the mobility of methane on the three substrates is not isotropic but is instead determined by the porous structure. As the adsorbate size increases, because of hindered diffusion, the diffusion coefficient decreases. Reasonable agreement was observed between the predicted diffusivities and experimental pulse field gradient NMR data (Briscoe et al. 1988). This contribution demonstrates the advantage of molecular simulations compared to experiments, as this computational approach allows researchers to identify the preferential trajectories for each adsorbed species, thus allowing a complete understanding of the properties of the confined fluids and how such properties depend on the morphology, chemical composition, etc., of the confining pores. Of course, satisfactory comparison to experiments is needed to ratify the reliability of the physical picture obtained.

As the computational capabilities evolved, it became possible to study the diffusion of linear and branched alkanes on various zeolites, and even to calculate the activation energies by producing Arrhenius-type plots (Webb et al. 1999). The models implemented to describe the zeolites have also become more and more realistic. Webb et al. (1999) showed that the geometry of the pores, the presence of protrusions, and that of void spaces along the channel walls strongly influence the diffusion coefficient, as well as the activation energy for diffusion of linear alkanes. The effects become even more pronounced when the alkane chains are branched (the branched alkanes simulated in this contribution contained one methyl group linked at various positions along the otherwise linear chain). The calculations were performed at low loadings and for up to 40 ns. Skoulidas and Sholl (2002) extended these types of calculations,

and investigated the effect of loading on the self-diffusion coefficient of small molecules (methane, helium, and argon) within silicalite. The results, in good experimental agreement, showed that the diffusion coefficient decreases as the loading increases. These authors also used the self-diffusion coefficients results to estimate transport diffusivities. The latter data have been instrumental for developing theoretical models to predict the permeability of zeolite membranes to various gases (Newsome and Sholl 2005).

Regarding studies on the effect of loading on permeability, it is worth remembering that Raghavan and Macelroy (1995) conducted equilibrium MD simulations for short alkanes adsorbed within models of silica gels at low loadings. They characterized the structure of the films adsorbed onto the solid substrate as a function of temperature. They found that the adsorbed hydrocarbon chains are characterized by a substantial broadening of the bond angle and dihedral angle distributions compared to the same molecules in the bulk. They also found that the diffusivity of the adsorbed chains increases as the loading increases because of screening of the fluid-pore interactions due to the pre-adsorbed molecules.

The simulation studies summarized here could be a starting point for addressing experimental observations of relevance for applications such as CO₂ sequestration. Key reactions and chemical mass transfer rates associated with progressive water-CO₂-rock interactions can be assessed by batch experiments such as those conducted by Gysi and Stefansson (2012). These authors conducted batch experiments at 40 °C for up to 260 days for four mineral assemblages: A1 – mixtures of Ca-Mg-Fe carbonates and altered basaltic glasses; A2 – Fe hydroxides and/or oxyhydroxides; A3 – mixtures of Ca-Mg-Fe clays and altered basaltic glasses; and A4 – mixtures of Ca-Fe clays and altered basaltic glasses. They maintained these samples at contact with water containing different amounts of initial dissolved CO₂ (ranging from 24 to 305 mmol/Kg). Then they monitored the concentration of the various species in the aqueous phase as a function of time. The results, summarized in Figure 29, suggest that increased aqueous CO₂ concentrations modify considerably the natural water-basalt reaction pathways during CO₂ mineralization. Equilibrium studies for the preferential adsorption of various compounds on the rock surfaces, such as those briefly described here, coupled with appropriate *ab initio* DFT studies could be useful for better understanding such phenomena at conditions of geological importance.

Simulation details

The interested reader is referred to specialized textbooks for a detailed discussion on simulation methods and algorithms (Nicholson and Parsonage 1982; Allen and Tildesley 1987; Frenkel and Smit 2002). This section is intended to summarize briefly some of the methods available to simulate systems of interest to subsurface applications, some of the models available to simulate alkanes, those that can be used to describe the solid substrate, and some of the experimental information that could validate the simulation results.

To study the properties of confined fluids from a theoretical/simulation perspective, a number of alternatives exist. The structure of confined fluids, as well as adsorption isotherms, can be calculated using classical density functional theory (Evans 1992) and integral equation theory (Henderson 1992) approaches. Both approaches require involved calculations for the minimization of the free energy, and often invoke approximations. An alternative, which is becoming widely accepted, is based on molecular simulations (Nicholson and Parsonage 1982). This latter approach is computationally expensive, and its reliability depends on the accuracy of the force fields implemented. It has the advantage of providing quantities that can be directly compared to experiments (e.g., self-diffusion coefficients, orientation of molecules near a substrate, radial distribution functions, vibrational frequencies, etc.). Very often molecular simulations are conducted within the MD formalism. However, it should be remembered that MD suffers from the difficulty of testing whether true equilibrium has been achieved. For example, the chromatography community has shown that MD simulations for confined systems

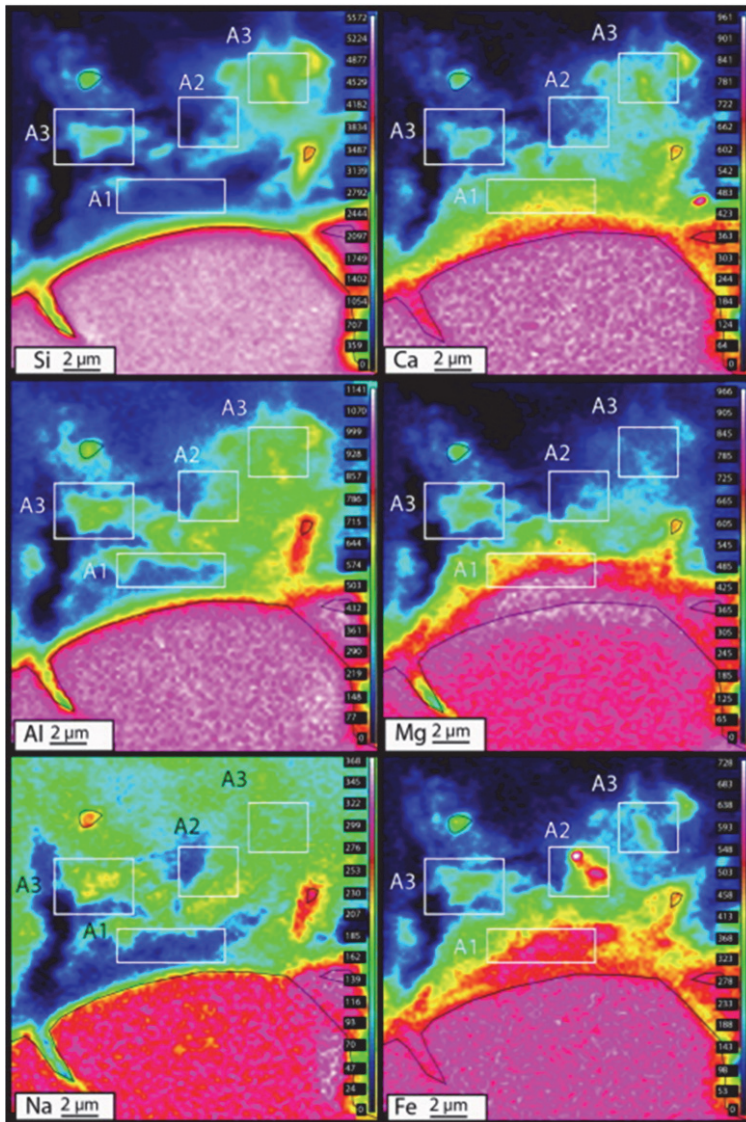


Figure 29. Elemental composition of mineral assemblages after a reaction time of 30 days. The samples were exposed to aqueous solutions with initial concentration of $\text{CO}_2 < 50 \text{ mmol/Kg}$, and maintained at 40°C . Compared to fresh basaltic glasses, A1 assemblages are depleted in Si, Al, and Na and enriched in Ca, Mg, and Fe; A2 assemblages are enriched in Fe and depleted of all other elements; A3 and A4 assemblages are enriched in Si, Al, Na, Ca, Mg, and Fe, although sometimes the amount of Na and Mg was found to be moderate. [Used by permission of Elsevier Pub © 2012, from Gysi and Stefansson (2012) *Geochim Cosmochim Acta*, Vol. 81, Fig. 9, p. 140.]

containing alkanes (in their case grafted to a silica substrate) and water are strongly influenced by the initial configurations (Klatte and Beck 1996; Schure 1998). Specifically, it was found that for water it is difficult to permeate hydrocarbon chains that have previously collapsed onto a silica substrate. Monte Carlo techniques provide more reliable results, independent of the initial configuration (Zhang et al. 2005).

An alternative approach to molecular simulations, which could be used to study the equilibrium properties of fluids confined within porous materials, is based on equations of state. These approaches are attractive because their analytical form provides quick estimates for phase equilibria and mixture composition, although they rely on rather strong simplifications for fluid-fluid and fluid-pore interactions and they cannot provide density distributions within the pores, nor dynamical properties for the confined species. However, they could be used to estimate the composition of the confined fluids, which is necessary to initiate more involved molecular dynamics simulations. The development of equations of states for confined fluids is due to numerous contributions. Zhu et al. (1999) considered fluids in cylindrical mesopores (e.g., MCM-41). Schoen and Diestler (1998) applied the perturbation theory to describe fluids in slit-shaped pores. Giaya and Thompson (2002) applied the latter methodology successfully to describe water in cylindrical pores. Zarragoicoechea and Kuz (2002) extended the van der Waals equation of state to fluids in square pores. Derouane (2007) further extended the approach and obtained agreement with experimental data for the reduction in the critical temperature compared to bulk values for the confined fluid (Derouane 2007). Travalloni et al. (2010) applied the van der Waals approach to model simple fluids and their mixtures confined in porous solids. The model manages to reproduce several adsorption isotherm types, successfully correlates to experimental data for pure hydrocarbons adsorbed in pores, and reasonably well predicts binary mixtures adsorption without the need of binary interaction parameters. The mixtures considered included toluene and 1-propanol in DAY-13 zeolites, and methane and ethane in MCM-41.

Models for alkanes. One model available to describe alkanes has been developed by Smith and coworkers both at the explicit and at the united-atom levels (Smith and Yoon 1994). With subtle modifications, this model has been used to study, for example, interactions between polymer nanofibers (Buell et al. 2010), and it reliably reproduces structural and dynamical properties of bulk alkanes. Alternative force fields for alkanes include the widely applied united-atom version of the transferable potentials for phase equilibria (TraPPE-UA; Martin and Siepmann 1998, 1999; Chen et al. 2001; Stubbs et al. 2004). Bolton et al. (1999) employed *ab initio* DFT to parameterize the interactions between the alkane model of Smith and coworkers and Al-terminated alumina substrates. They then compared the results obtained when either the explicit or the united-atom models were used to simulate octane at contact with alumina. The results suggest that when the structure of interfacial octane is considered, united-atom and explicit models yield comparable results. However, rotational and translational dynamics are not satisfactory when the united atom model is employed, suggesting the need of including an explicit description of the hydrogen atoms within the hydrocarbon chain.

Significant work has also been done in predicting the stability of clathrates in the water-methane system. Considering the selection of appropriate force fields, the contribution from Alavi et al. (2007) should be highlighted. These authors employed MD simulations and implemented careful free-energy calculation techniques to establish the occupancy of methane in H clathrate hydrates at 300 K and 2 GPa. They compared the OPLS united atom Lennard-Jones potential, the Tse-Klein-McDonald five-site force field, and the Murad-Gubbins five-site potential to describe methane. The results show that the force field implemented strongly influences the predicted occupancy. The OPLS and the Tse-Klein-McDonald models yield occupancy of 5 methane molecules per cage, while the Murad-Gubbins model yields smaller occupancy. The differences in the results are due to the less attractive methane-methane potentials implemented by the Murad-Gubbins model.

Models for the solid substrates. Solid mineral substrates can be simulated implementing the popular CLAYFF force field (Cygan et al. 2004b). However, it is suggested to validate the force field by reproducing known experimental observations for the system of interest. When interested in studying carbon-based materials, the interested reader could take advantage of the vast literature developed to study adsorption in realistic models of activated carbons (Petersen et al. 2003; Palmer et al. 2010). However, a rational effort to investigate the effect of confinement on the properties of alkanes and of their mixtures requires, in our opinion, the employment of simplified models (e.g., the slit-shaped pore), especially when mixtures are considered. One microscopic model that is simple enough to allow researchers to obtain meaningful insights, yet complex enough to reproduce important experimental observations, has been recently proposed by Kowalczyk et al. (2010). This model has proven successful in simulating the adsorption of small hydrocarbons, as well as that of mixtures containing hydrocarbons and hydrogen. The results are satisfactory when compared to experimental data obtained in carbon molecular sieves. Additionally, the anomalous transport of small molecules (hydrogen vs. methane) in carbon molecular sieves can be explained by using this model. It was found that the size of the nanopore constrictions determines the anomalous diffusion, while the size of the cages does not influence the transport properties of the confined fluids.

Validation of simulation predictions. When possible, simulation data should be compared to desorption energies estimated from temperature-programmed desorption experiments (Slayton et al. 1995), chromatographic results, and batch techniques (Partyka and Douillard 1995; Askin and Inel 2001; Dabrowski et al. 2003; Diaz et al. 2004). Electron energy loss spectroscopy (Machida et al. 2002) and attenuated total reflection Fourier transform infrared spectroscopy (ATR-FTIR) (Dubowski et al. 2004; Almeida et al. 2008) can be used to study surface species on flat surfaces. Raman (Resini et al. 2005; Kim and Stair 2009) and transmission IR (Mawhinney and Yates 2001; Yeom et al. 2004) spectroscopies could provide information for hydrocarbons adsorbed on high-surface-area powders. One technique that is becoming very popular for studying structural details of molecules with any orientation with respect to an interface is the vibrational sum-frequency generation (SFG), which has been used previously to study molecules on oxide surfaces (Nanjundiah and Dhinojwala 2005; Hayes et al. 2009; Stokes et al. 2009). For instance, Sefer et al. (1995) studied liquid hexadecane at the silica interface, and found a preferential orientation parallel to the interface. Buchbinder et al. (2010) studied linear and cyclic alkanes and alkenes at the liquid-alumina interface. The results show that liquid alkanes, both linear and cyclic, prefer to lay parallel to the solid substrate. On the contrary, unsaturated olefins did not show consistent trends. As noted above, the diffusion constant of gases in pores can be measured experimentally by conducting macroscopic uptake rate measurements and microscopic ones by conducting pulsed field gradient nuclear magnetic resonance (PFG NMR) and quasi-elastic neutron scattering (Kärger and Ruthven 1991; June et al. 1992; Maginn et al. 1996; Reyes et al. 1997; Runnebaum and Maginn 1997). In our opinion microscopic observations (e.g., NMR and/or neutron scattering) are preferable to macroscopic ones, because they provide a direct comparison to the results predicted by simulations.

SUMMARY AND RECOMMENDATIONS

An atomistic to molecular-level understanding of how C-O-H fluids (e.g., water, CO₂, CH₄, higher hydrocarbons, etc.) interact with and participate in reactions with other solid Earth materials is central to the development of predictive models that aim to quantify a wide array of geochemical processes. The importance of the adsorption, microstructure and dynamics of important hydrocarbon and related fluids has been highlighted as well as the sensitivity of C-O-H fluid species to perturbations by a change in physical conditions or proximity to solute molecules and interfaces. Despite the large body of work that documents the nature of these processes and associated interactions with its local surroundings, it is premature to assume that

we have a complete understanding of the mechanisms that give rise to the particular properties exhibited by hydrocarbon fluids. Understanding is more limited as one goes both above and below ambient conditions. For example, there is continuing discussion on the metastability of hydrocarbon species as a system experiences more extreme elevated temperature and pressure relevant to deep Earth environments. This is of particular interest, since we have seen that nanoporous confinement of C-O-H fluids at ambient conditions leads to structural and dynamical features that deviate markedly from bulk system behavior. In the context of natural systems, interrogation of fluids and fluid-solid interactions at elevated temperatures and pressures is an area requiring much more work, particularly for complex solutions containing geochemically relevant aqueous species interacting with relevant C-O-H fluids within the interfacial regime. We have tried to describe a series of prototypical interfacial and surface problems using a number of examples to stimulate the thinking of Earth scientists interested applying some of these outcomes to confined systems of mineralogical importance.

Our ability to predict the molecular-level properties of fluids and fluid-solid interactions relies heavily on the synergism between novel experiments, such as neutron scattering or nuclear magnetic resonance and molecular-based simulations. Tremendous progress has been made in closing the gap between experimental observations and predicted behavior based on simulations, owing to improvements in the experimental methodologies and instrumentation on the one hand, and the development of new potential models for C-O-H fluid species on the other. There has been an emergence of studies taking advantage of advanced computing power that can accommodate the demands of *ab initio* molecular dynamics. On the neutron instrumentation side, while much of the quasi-elastic work described above has been performed using instrumentation located at reactor based sources, the advent of second-generation spallation neutron sources like ISIS, new generation sources like the SNS at the Oak Ridge National Laboratory, and the low repetition rate second-target station at ISIS now offer significant opportunities for the study of interfacial and entrained liquids. Development of unique sample cells that allow interrogation of higher temperature-pressure conditions relevant to crust and mantle settings are needed that can allow interrogation of complex fluid-solid interactions. An improvement of the counting statistics by one to two orders of magnitude on many instruments, such as vibrational and time-of-flight spectrometers at SNS, will allow parametric studies of many hydrocarbon-based systems that otherwise would be prohibitively time consuming. The extended- Q SANS diffractometer and liquids reflectometer at SNS will offer very high intensity and unparalleled Q -range to extend the accessible length scale in real space, from 0.05 nm to 150 nm. The backscattering spectrometer will provide very high intensity and excellent energy resolution through unprecedented range of energy transfers, thereby allowing simultaneous studies of translational and rotational diffusion components in various systems. The vibrational spectrometer, with two orders of magnitude improvement in performance and the capability to perform simultaneous structural measurements, should present exciting opportunities as well, and support a new population of users interested in quantifying behavior of hydrocarbons and other fluid species relevant to Deep Earth.

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